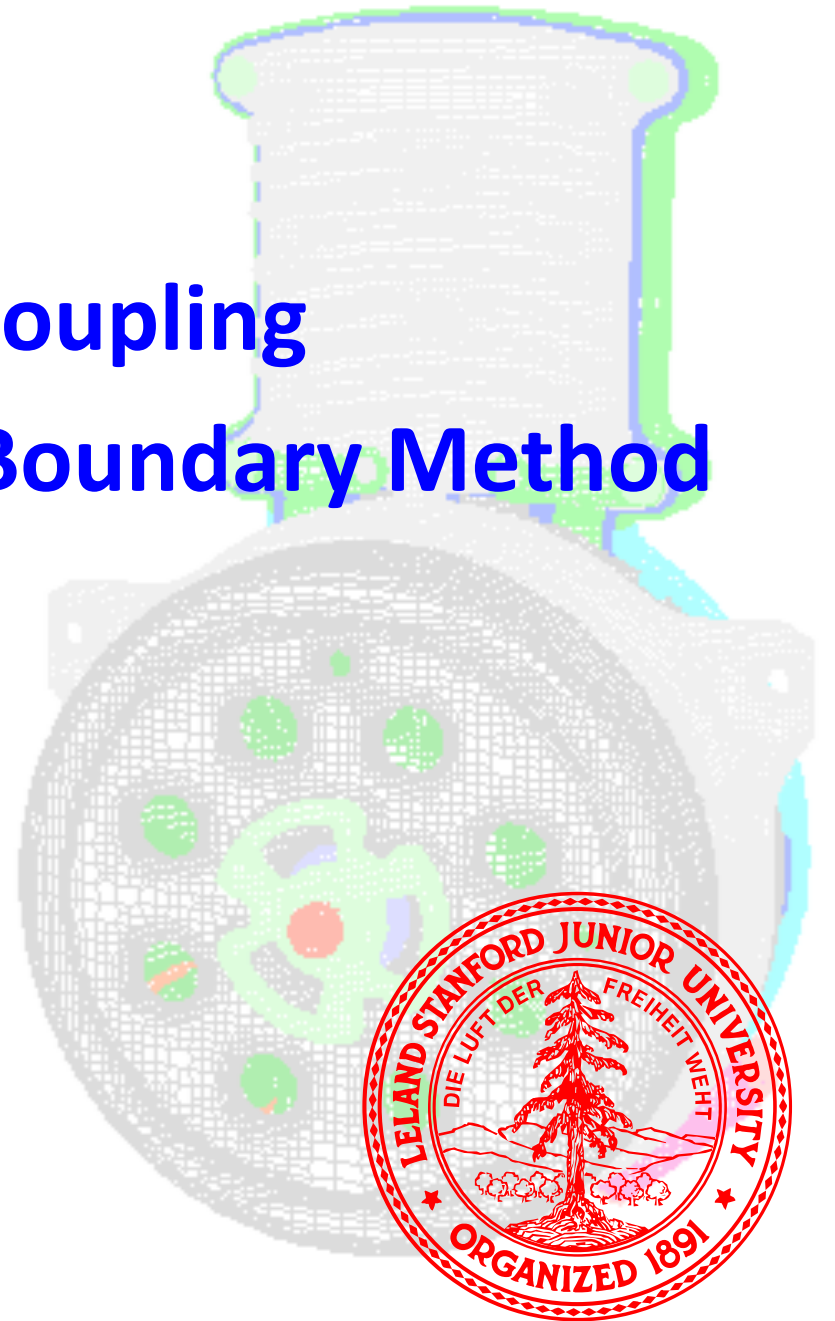


Solid/Fluid Thermal Coupling Using the Immersed Boundary Method

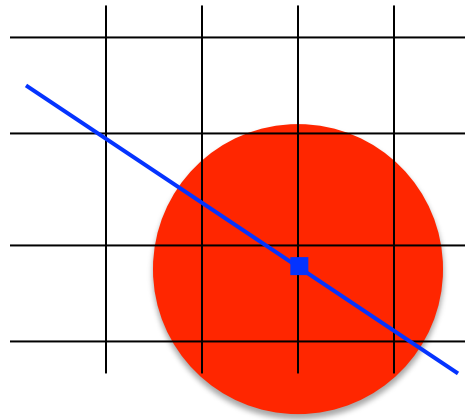
Gianluca Iaccarino
Mechanical Engineering
Stanford University

XXXV WSC Conference
October 6-10, 2010, Zeist, The Netherlands.

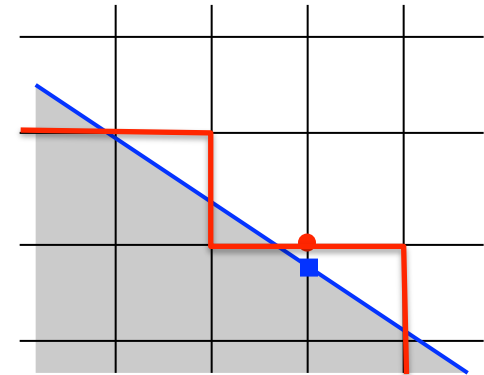


Non-Body-Fitted Approaches

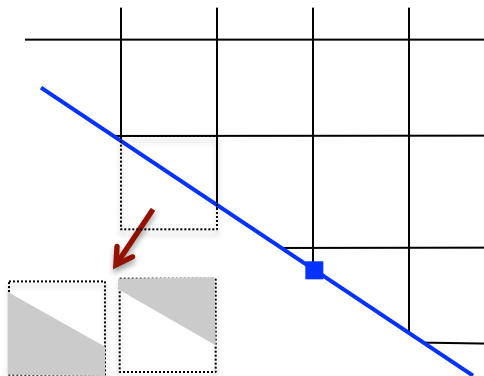
- True Boundary



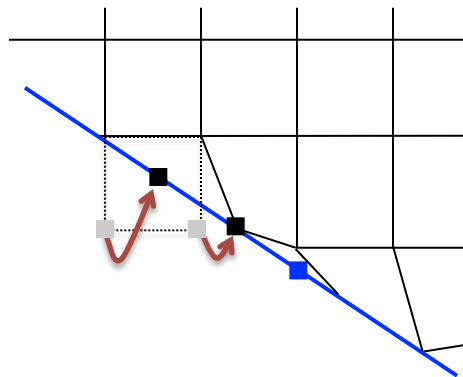
IB with Forcing



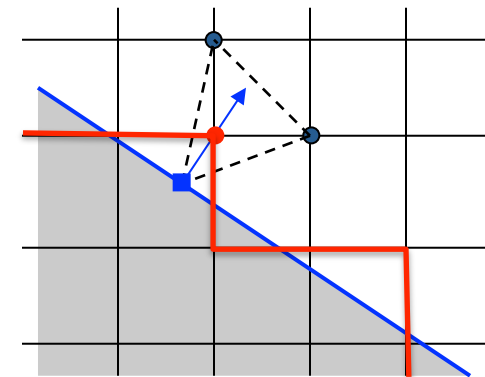
Stairstep/Mask



Cut-Cell (Body-Fitted)



Projection (Body-Fitted)
OpenFoam SnappyHex



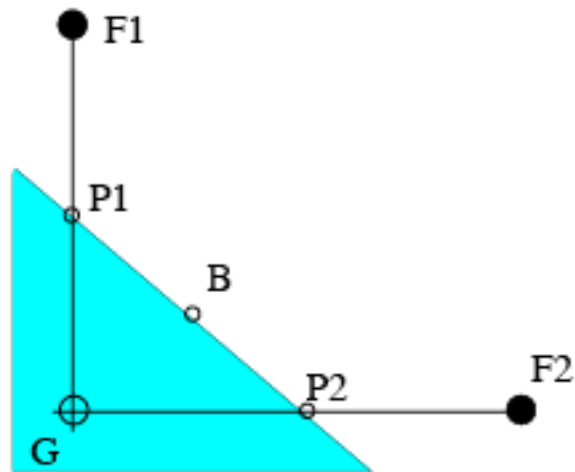
IB reconstruction

4. IB Reconstruction

Solid/Fluid Thermal Coupling
Using the Immersed Boundary Method

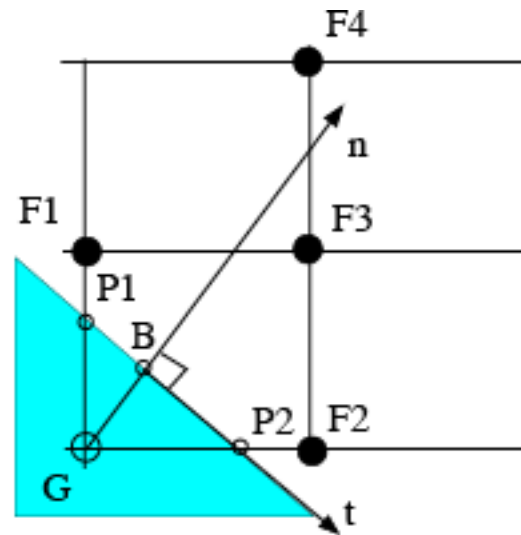
Geometric IB Reconstruction

Linear Reconstruction



$$\phi = a_1 x + a_2 y + a_3$$

Quadratic Reconstruction

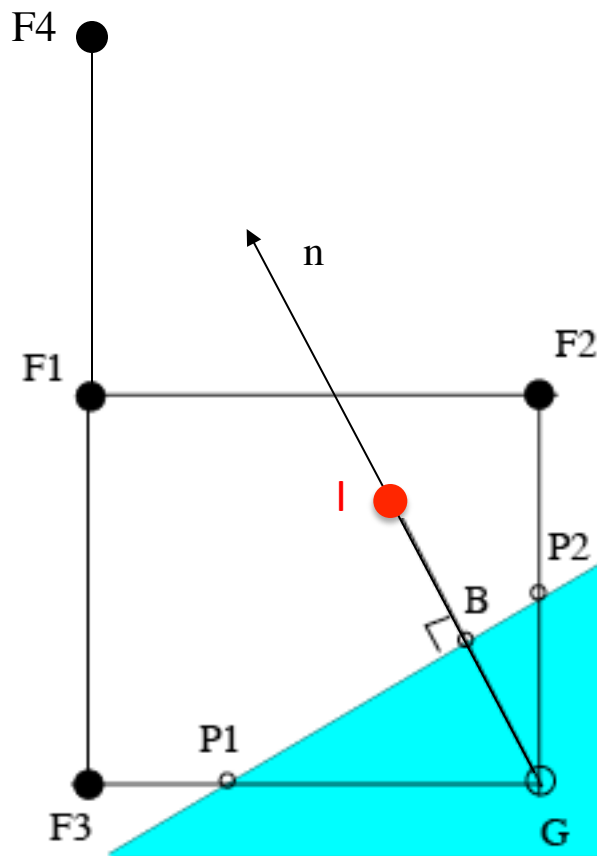


$$\phi = a_1 n^2 + a_2 n + a_3 t + a_4 nt + a_5$$

F: fluid points; B: boundary point; G: ghost point

Geometric IB Reconstruction

The quadratic reconstruction scheme requires 4 fluid nodes + BC



Remarks:

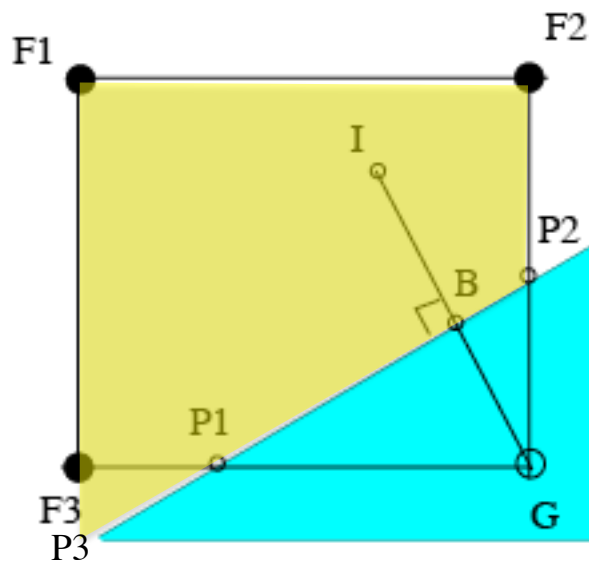
- 1) The fluid points F1-F4 are selected according to the angle between the IB and the grid
- 2) The image point is used to construct the interpolation and then the boundary value is reflected

F: fluid points; B: boundary point;
G: ghost point; I: image of the ghost point

Physics-based IB Reconstruction

The quadratic reconstruction scheme requires 4 fluid nodes + BC

We can build a **better reconstruction** by using the conservation of momentum in a “ghost” control volume
(4 fluid nodes + BC + conservation of mass)



$$\phi = a_1 n^2 + a_2 n + a_3 t + a_4 nt + a_5$$

$$U (P2-F2) - U (P3-F1) + V (F1-F2) = 0$$

F: fluid points; B: boundary point;
G: ghost point; I: image of the ghost point
P: Additional surface points

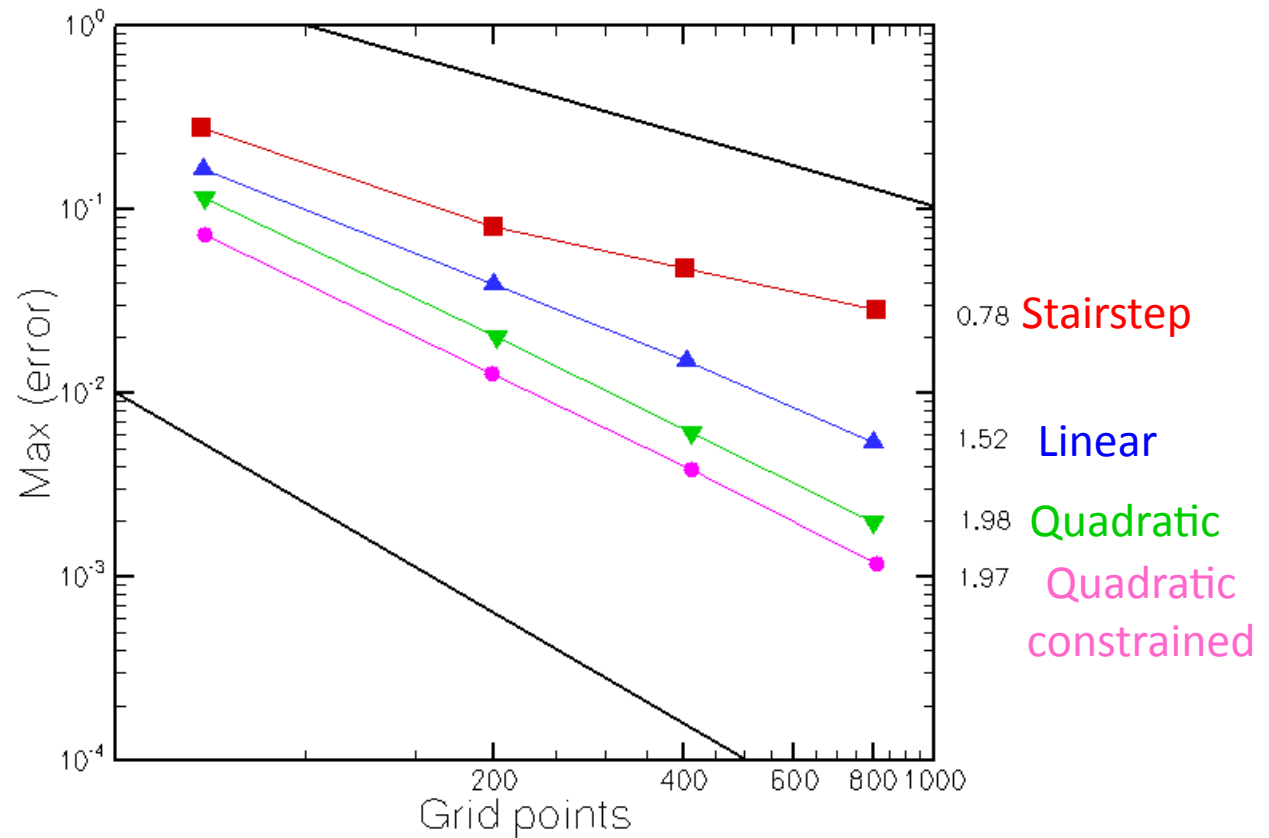
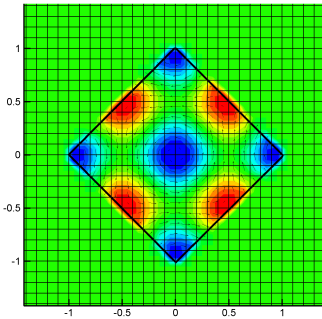
Verification Test

Decaying vortex problem (exact solution of the Navier Stokes equations)

$$p(x, y, t) = -\frac{1}{4}(\cos 2\pi x + \cos 2\pi y) e^{-4\pi^2 t / \text{Re}}$$

$$u(x, y, t) = -\cos \pi x \sin \pi y e^{-2\pi^2 t / \text{Re}}$$

$$v(x, y, t) = \sin \pi x \cos \pi y e^{-2\pi^2 t / \text{Re}}$$

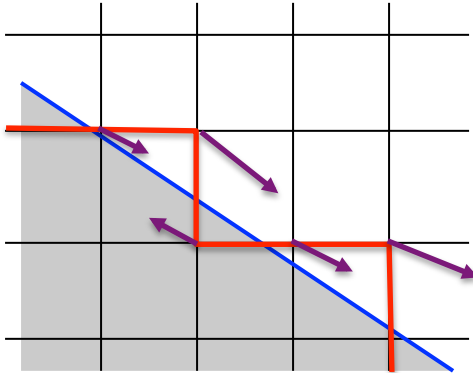


Achieved **2nd order accuracy** at the Immersed Boundary

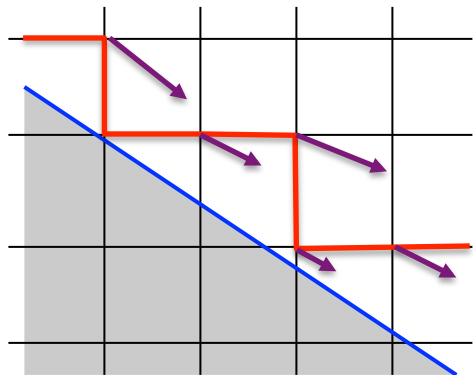
Reconstruction Schemes

- **Flow in an impeller stirred tank using an immersed boundary method.**
R. Verzicco, G. Iaccarino, M. Fatica and P. Orlandi, CTR Annual Briefs ,2000
1D linear, low-Re flow
- **RANS solver with adaptive structured boundary non-conforming grids**
S. Majumdar, G. Iaccarino and P. Durbin, CTR Annual Briefs ,2001
2D linear & quadratic, image point reflection, laminar flow
- **Turbulence modeling in an immersed-boundary RANS method**
G. Kalitzin and G. Iaccarino, CTR Annual Briefs ,2002
3D linear & inverse distance, turbulent flow, RANS
- **Wall modeling for large-eddy simulation using an immersed boundary method**
F. Tessicini, G. Iaccarino, M. Fatica, M. Wang and R. Verzicco, CTR Annual Briefs , 2002
3D linear/logarithmic, turbulent flow, LES
- **Accurate and efficient immersed-boundary interpolations for viscous flows**
S. Kang, G. Iaccarino and P. Moin, CTR Annual Briefs, 2004
3D linear & quadratic, mass conservation constant, turbulent flow, LES
- **Immersed boundary for compressible flow simulations on semi-structured meshes**
M. de Tullio and G. Iaccarino, CTR Annual Briefs , 2005
3D linear & quadratic, compressible, turbulent flow, RANS
- **Automatic mesh generation for LES in complex geometries**
G. Iaccarino and F. Ham, CTR Annual Briefs , 2005
3D linear, local and global mass conserving reconstructions, turbulent flow, LES

Mass Conservation



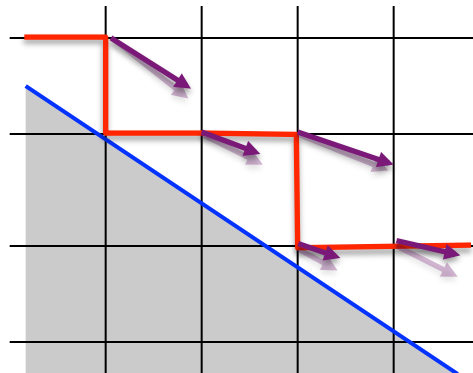
The Reconstructed stencils reflect the velocity at the ghost points...this can lead to large velocity divergence close to the boundary and pressure oscillations



Forcing the IB “inside” the fluid domain eliminates the reflection!

However, The **Reconstructed velocity** at the virtual boundary still does not exactly conserve mass

$$(\vec{V} \cdot \hat{n})_{IB} \neq 0 \quad \text{both locally and globally}$$



We can define a correction of the reconstruction based either on the **global** mass imbalance

$$\propto \sum (\vec{V} \cdot \hat{n})_{IB} A_{IB} \quad \text{equally distributed at the IB nodes}$$

or the **local** mass flux $(\vec{V} \cdot \hat{n})_{IB}$

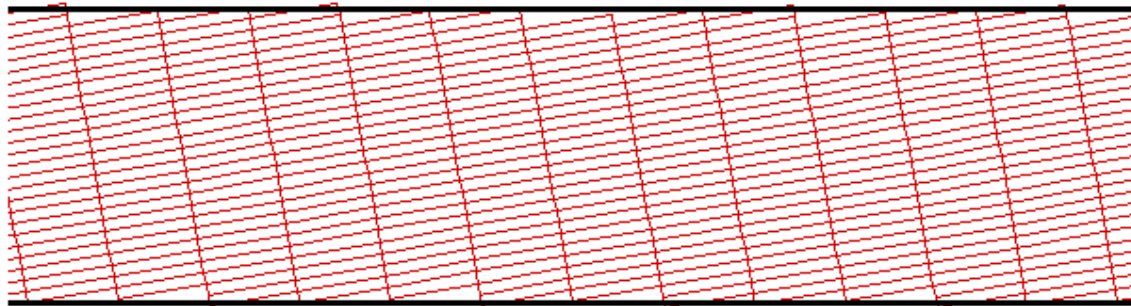
Laminar Channel

Use **Cartesian grids** generated in a rotated axis

- Periodic domain (no boundary conditions)
- Uniform grids (no effects of the numerical accuracy)

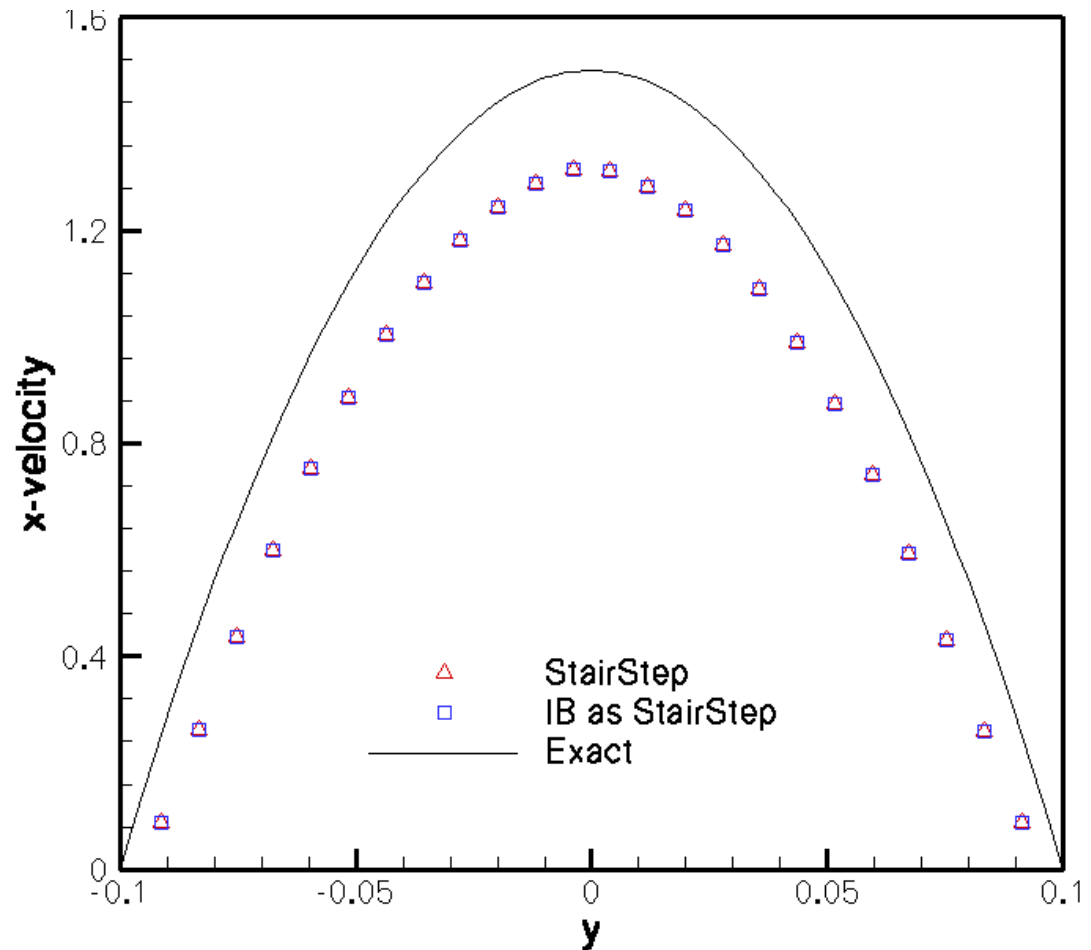
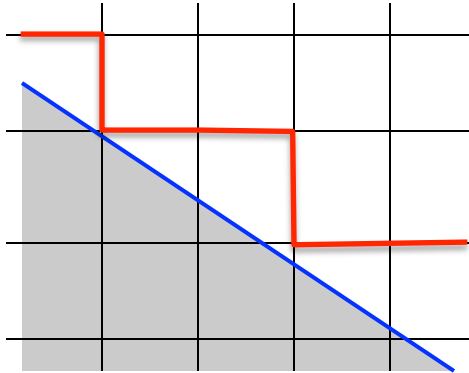
Test accuracy, symmetry, convergence

Used $\alpha = 20, 10, -10$ and three grid resolutions



$\alpha = 10$

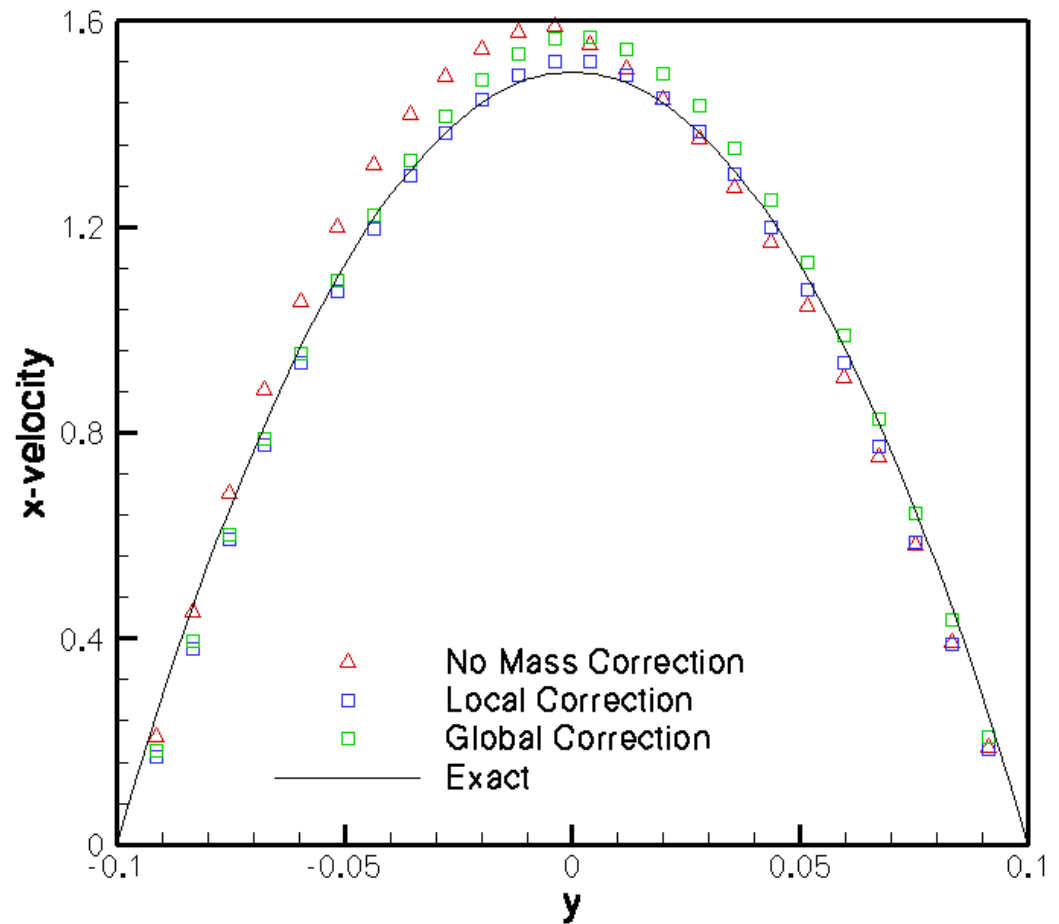
StairStep Solution



Remark: ibwalls are always inside the computational domain, hence we always obtain lower mass through (fixed pressure gradient!)

Mass Conservation

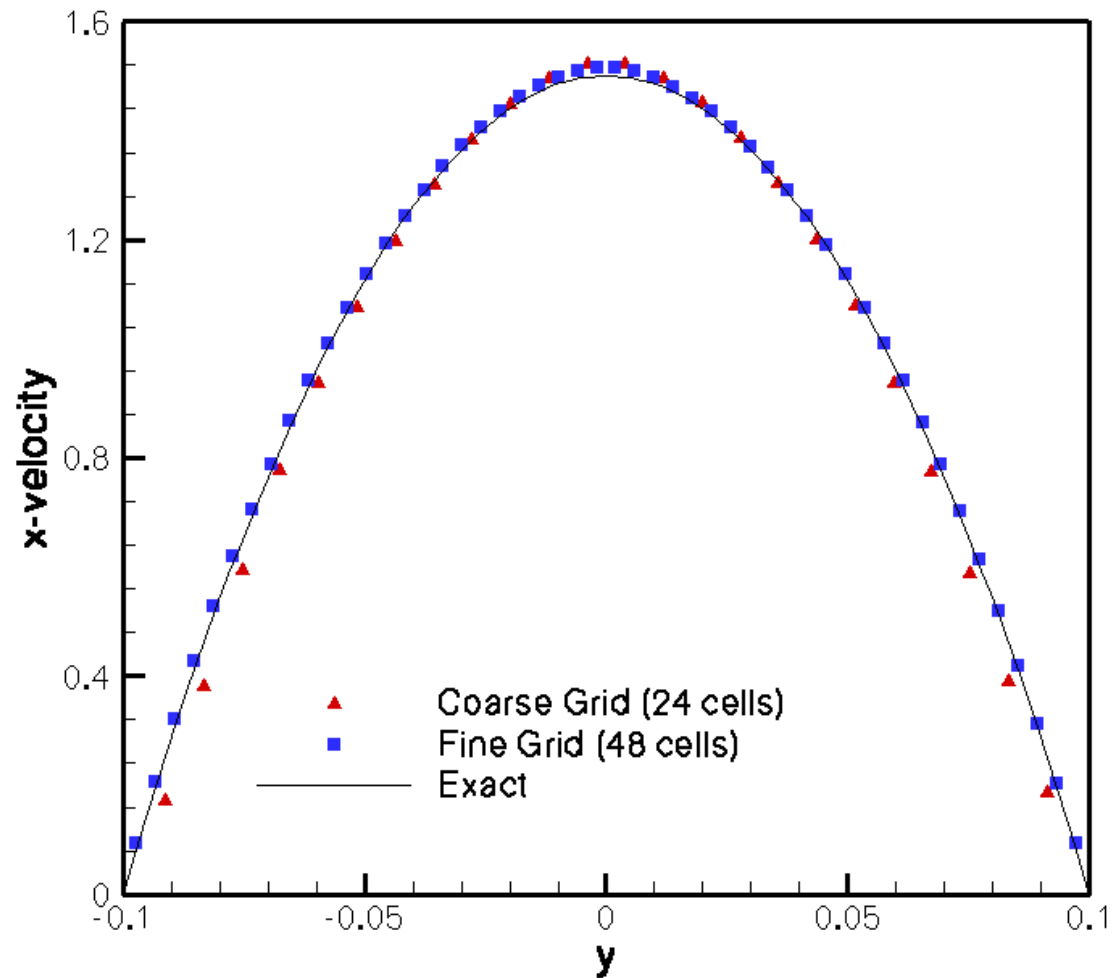
Effect of the mass correction applied to the ibwall interpolation
(Quadratic reconstruction)



Remark: the asymmetry is related to the grid not being top/bottom symmetric. The corrections eliminate it almost completely!

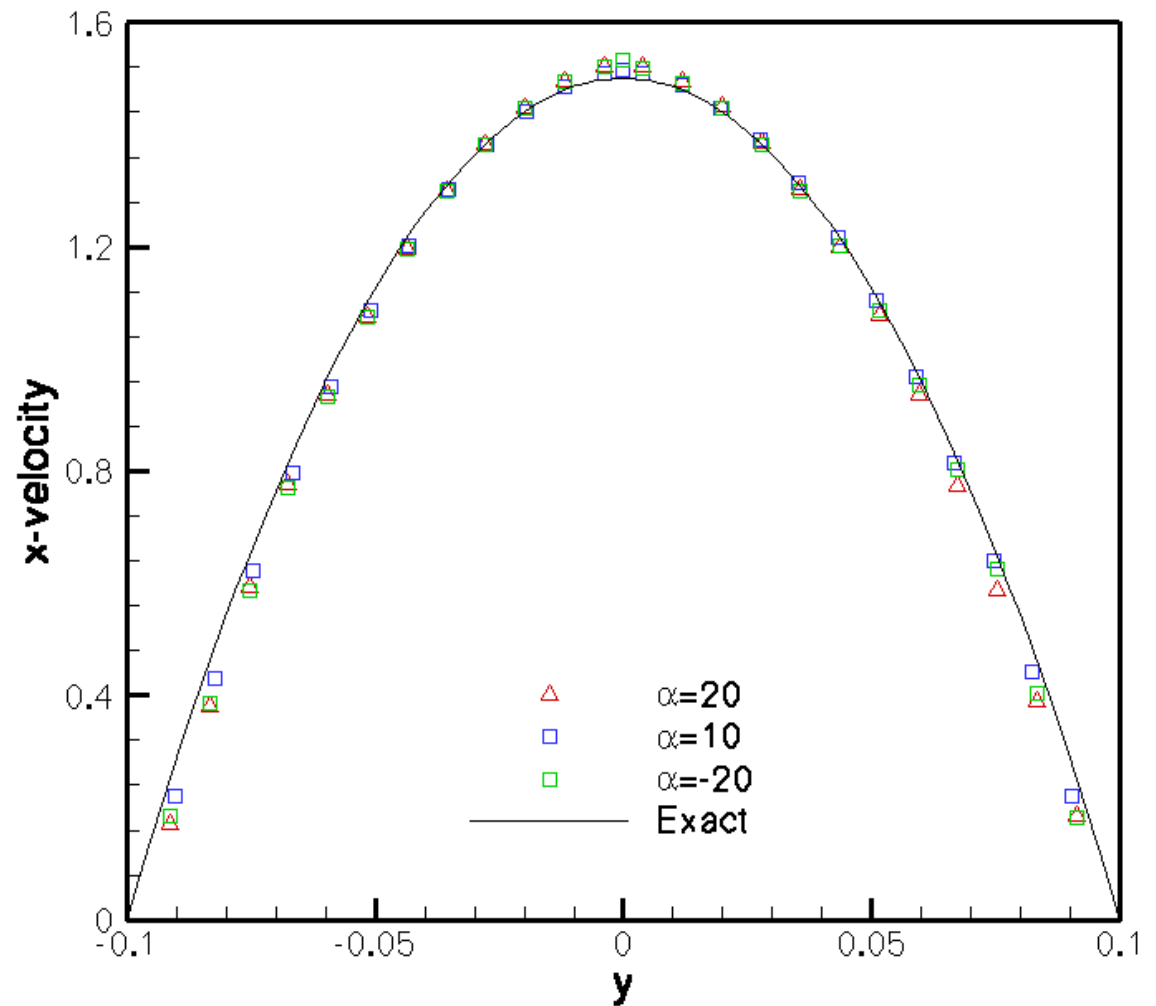
Grid Sensitivity

The solution correctly converges independently of the mass correction used.



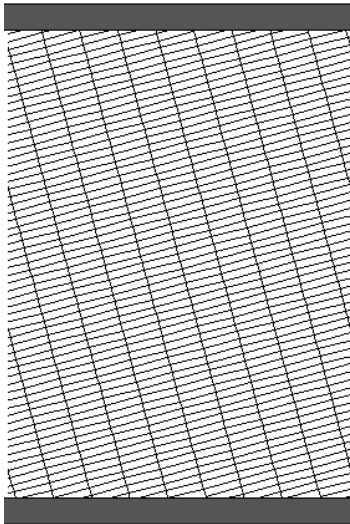
Grid Angle Sensitivity

Local mass correction provides a symmetric profile independently of the angle

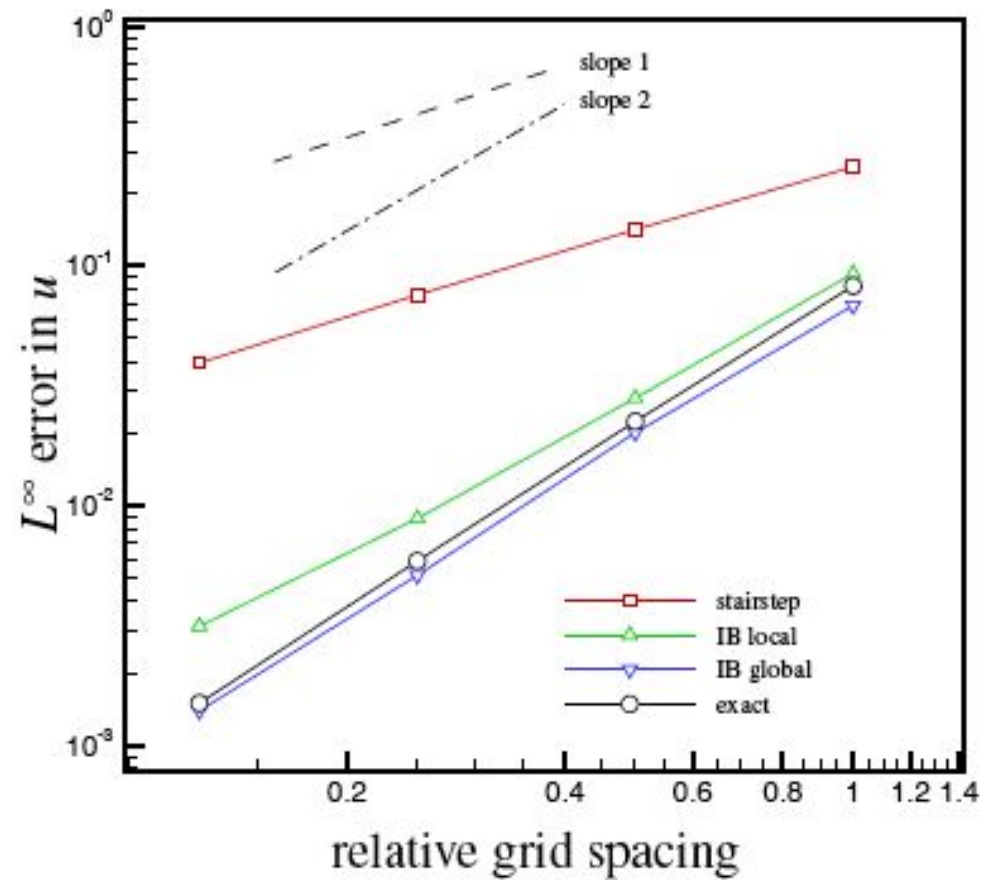


Verification Test

L^∞ error in velocity



$\alpha = 15^\circ$



Numerical Method - Details

Navier-Stokes Equations – Incompressible Fluid

$$\frac{\partial u_i}{\partial t} + \frac{\partial u_i u_j}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{1}{Re} \frac{\partial^2 u_i}{\partial x_j \partial x_j} \quad \text{Momentum}$$

$$\frac{\partial u_i}{\partial x_i} = 0 \quad \text{Continuity}$$

Fractional Step Method – Crank-Nicholson in time, RK for Convective Terms

$$\left[\frac{1}{\Delta t} - \frac{(\alpha_k + \beta_k)}{2Re} \frac{\partial^2}{\partial x_j \partial x_j} \right] \hat{u}_i^k = \frac{u_i^{k-1}}{\Delta t} - (\alpha_k + \beta_k) \frac{\partial p^{k-1}}{\partial x_i} - \alpha_k \left(\frac{\partial u_i u_j}{\partial x_j} \right)^{k-1} - \beta_k \left(\frac{\partial u_i u_j}{\partial x_j} \right)^{k-2} + \frac{(\alpha_k + \beta_k)}{2Re} \left(\frac{\partial^2 u_i^{k-1}}{\partial x_j \partial x_j} \right) \quad \text{Momentum Predictor}$$

$$\frac{\partial^2 \phi}{\partial x_j \partial x_j} = \frac{1}{(\alpha_k + \beta_k) \Delta t} \frac{\partial \hat{u}_i^k}{\partial x_i} \quad \text{Diverge-free Constraint}$$

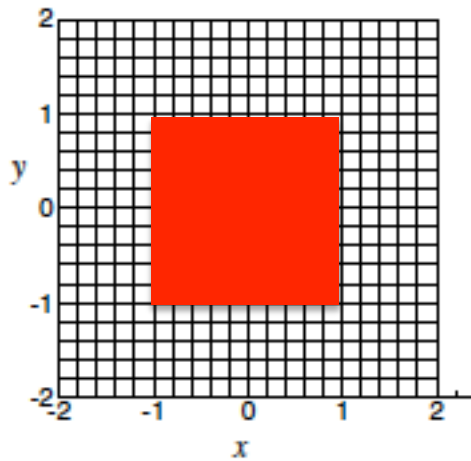
$$u_i^k = \hat{u}_i^k - (\alpha_k + \beta_k) \Delta t \frac{\partial \phi}{\partial x_i} \quad \text{Momentum Corrector}$$

$$p^k = p^{k-1} + \phi \quad \text{Pressure update}$$

IB Reconstruction

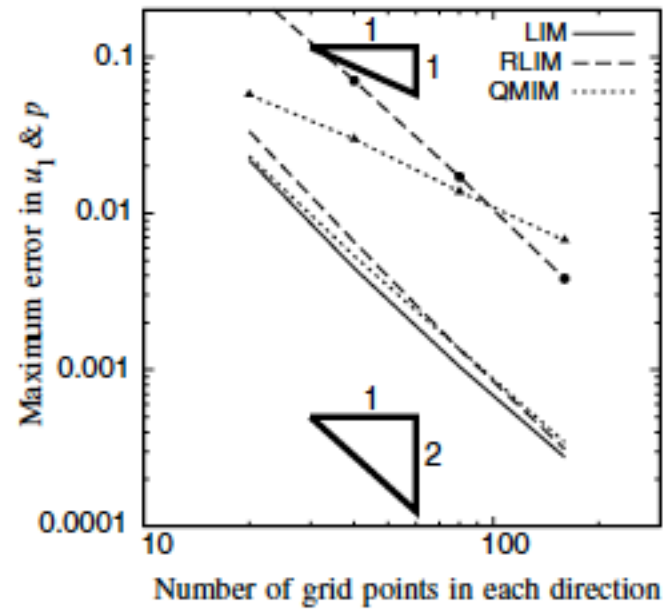
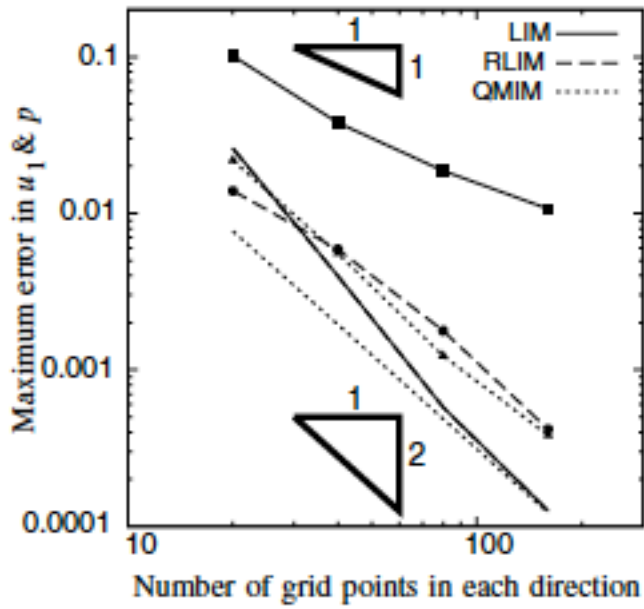
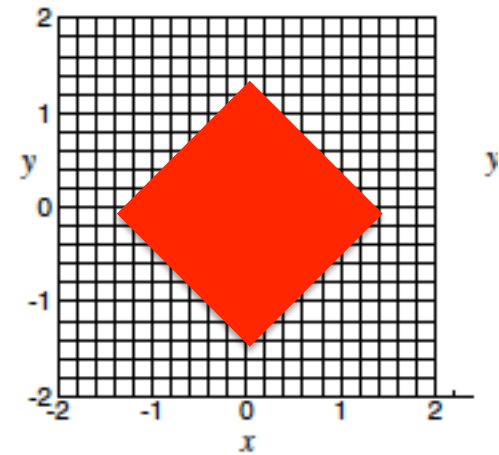
Linear	$u_{i,c}^k = \omega_{i,1} u_{i,1}^k + \omega_{i,2} u_{i,2}^k + \omega_{i,IB} u_{i,IB}^k$
Revised Linear	$u_{i,c}^k = \omega_{i,1} u_{i,1}^k + \omega_{i,2} u_{i,2}^k + \omega_{i,IB} u_{i,IB}^k$ $\Delta u_{i,c} = \omega_{i,1} \Delta u_{i,1} + \omega_{i,2} \Delta u_{i,2} + \omega_{i,IB} \Delta u_{i,IB}$ $\Delta u_{i,c} = \hat{u}_{i,c}^k - u_{i,c}^{k-1}$
Quadratic	$\hat{u}_i^k(x_1, x_2) = a_{i,1}^k x_1^2 + b_{i,1}^k x_1 + a_{i,2}^k x_2^2 + b_{i,2}^k x_2 + \hat{u}_{i,c}^k$
Quadratic + Momentum	$\hat{u}_i^k(x_1, x_2) = a_{i,1}^k x_1^2 + b_{i,1}^k x_1 + a_{i,2}^k x_2^2 + b_{i,2}^k x_2 + \hat{u}_{i,c}^k$ $\frac{\hat{u}_{i,c}^k}{\Delta t} - \frac{(\alpha_k + \beta_k)}{Re} (a_{i,1}^k + a_{i,2}^k) = \frac{u_{i,c}^{k-1}}{\Delta t}$ $- (\alpha_k + \beta_k) \frac{\partial p^{k-1}}{\partial x_i} - \alpha_k \left(\frac{\partial u_i u_j}{\partial x_j} \right)^{k-1}$ $- \beta_k \left(\frac{\partial u_i u_j}{\partial x_j} \right)^{k-2} + \frac{(\alpha_k + \beta_k)}{2Re} \frac{\partial^2 u_i^{k-1}}{\partial x_j \partial x_j}$

IB Reconstruction



Decaying Taylor Vortices

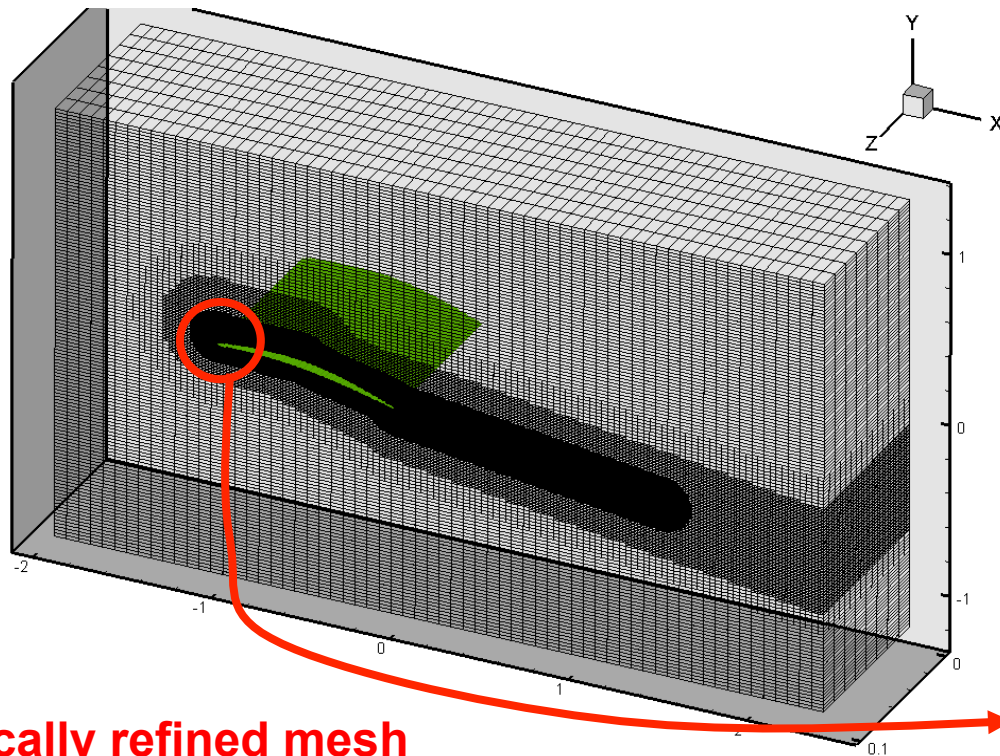
Exact Solution of NS Eqs.



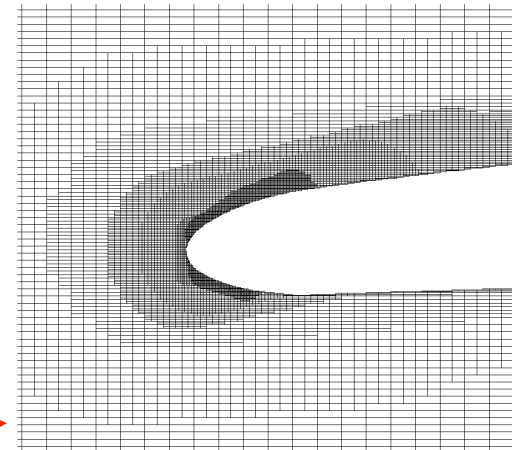
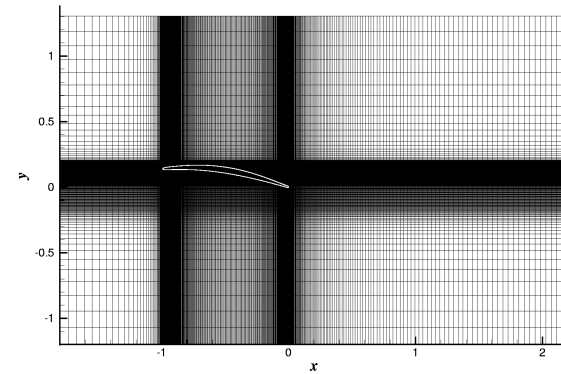
LES of airfoil flow

Re \sim 150,000 - Grid size \sim 7M

Local mesh refinement technique reduces the total number of mesh points by 70% compared to a (single-block) Cartesian mesh with similar mesh resolution near the wall



Cartesian mesh

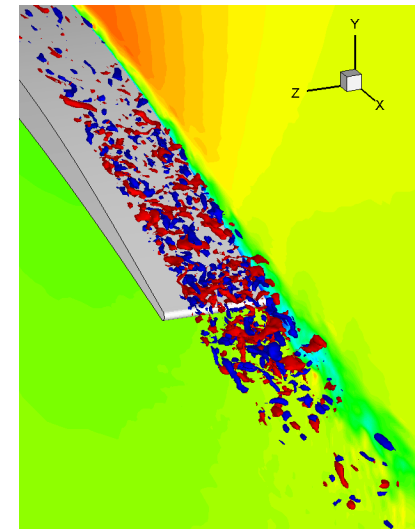
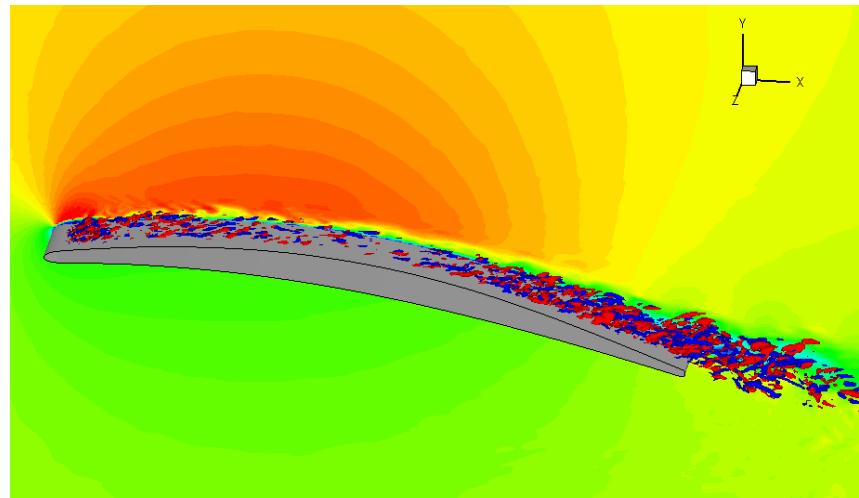
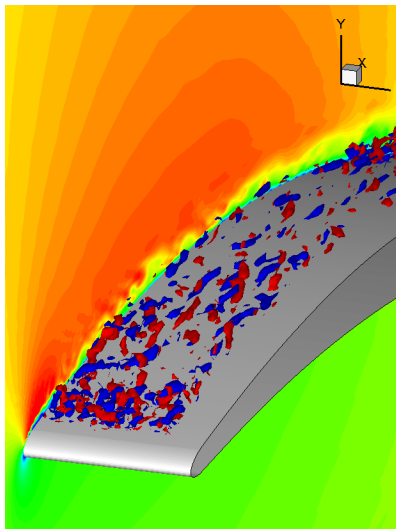


Locally refined mesh

LES of airfoil flow

Re \sim 150,000 - Grid size \sim 7M

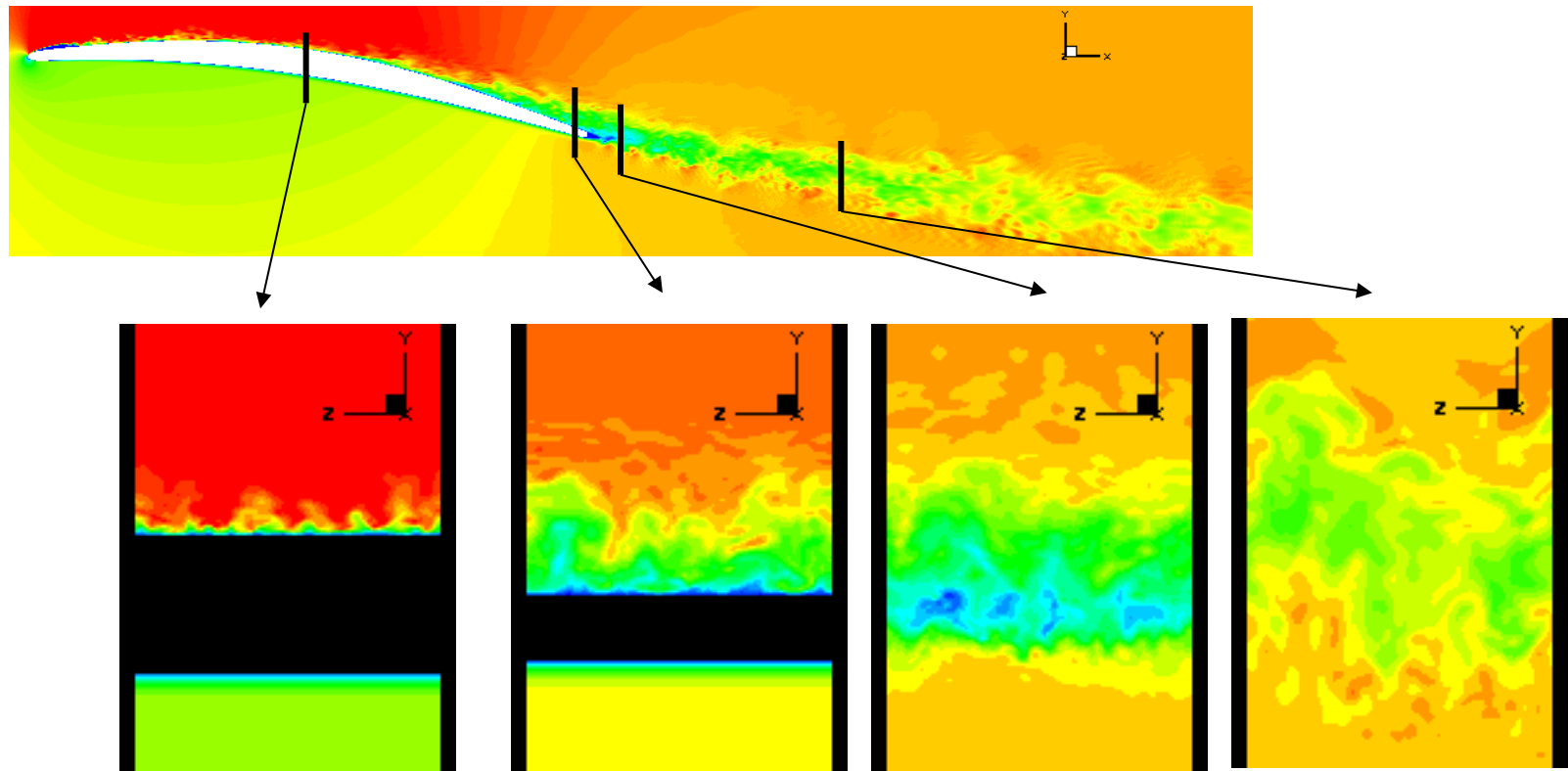
Small separation bubble near LE prompts transition to turbulence



Instantaneous x -velocity and x -vorticity

LES of airfoil flow

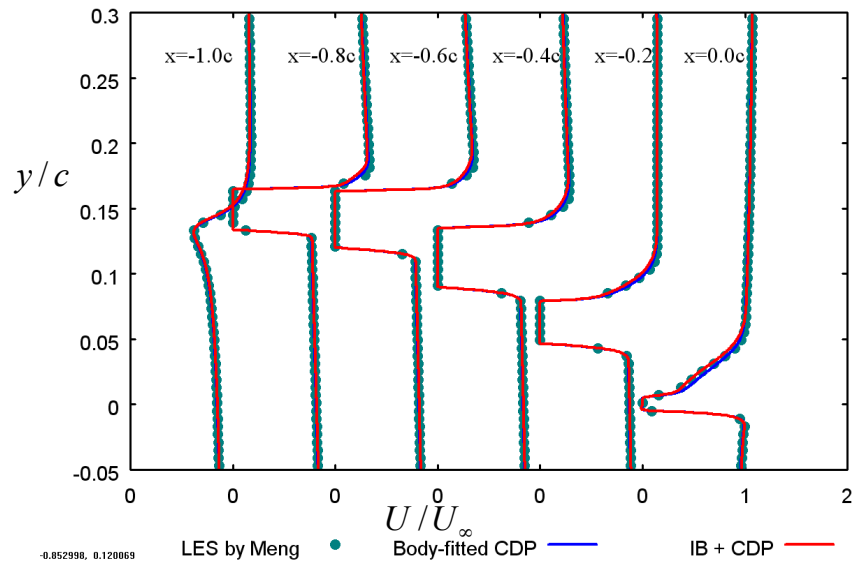
Re \sim 150,000 - Grid size \sim 7M



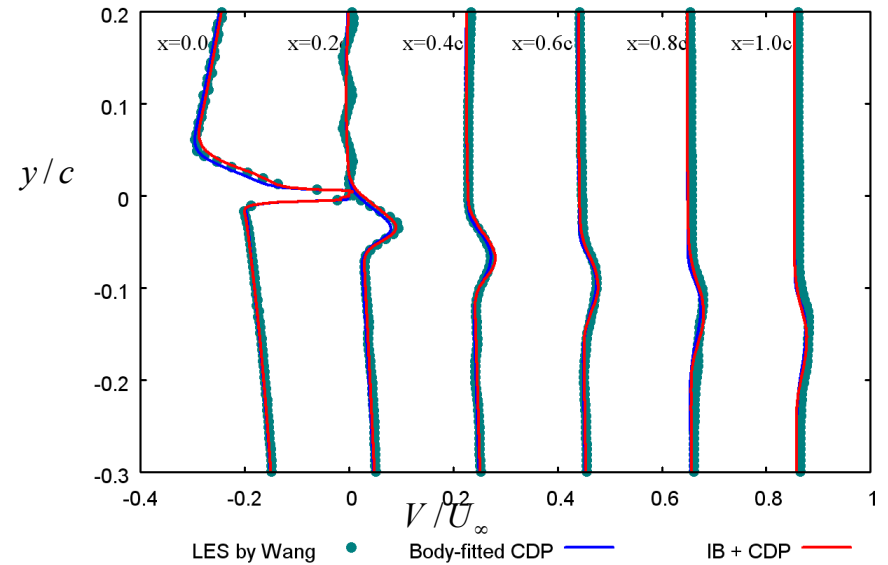
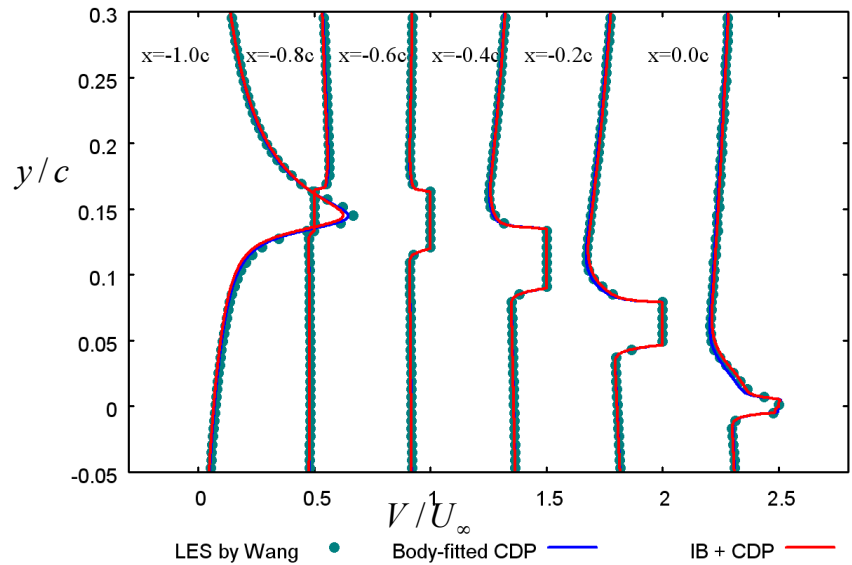
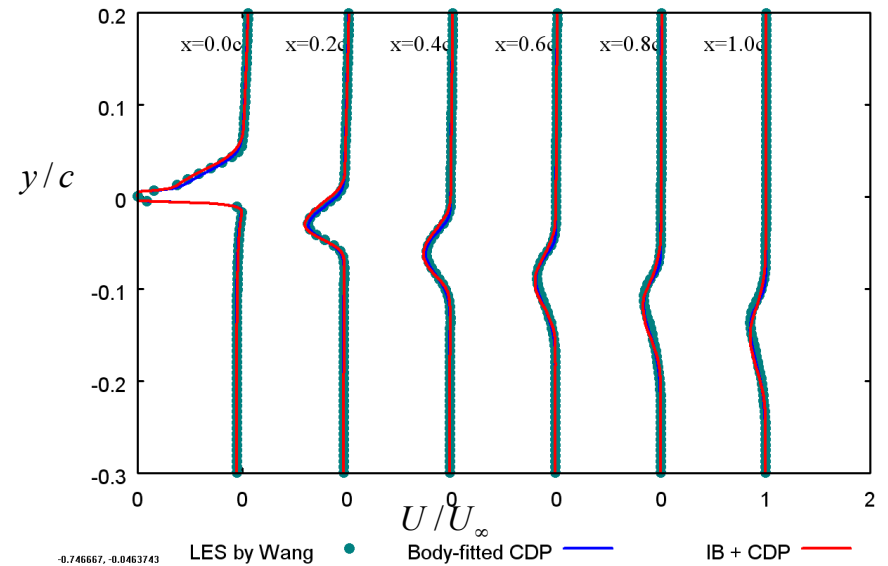
Streamwise velocity

Mean Flow Predictions

Over the airfoil



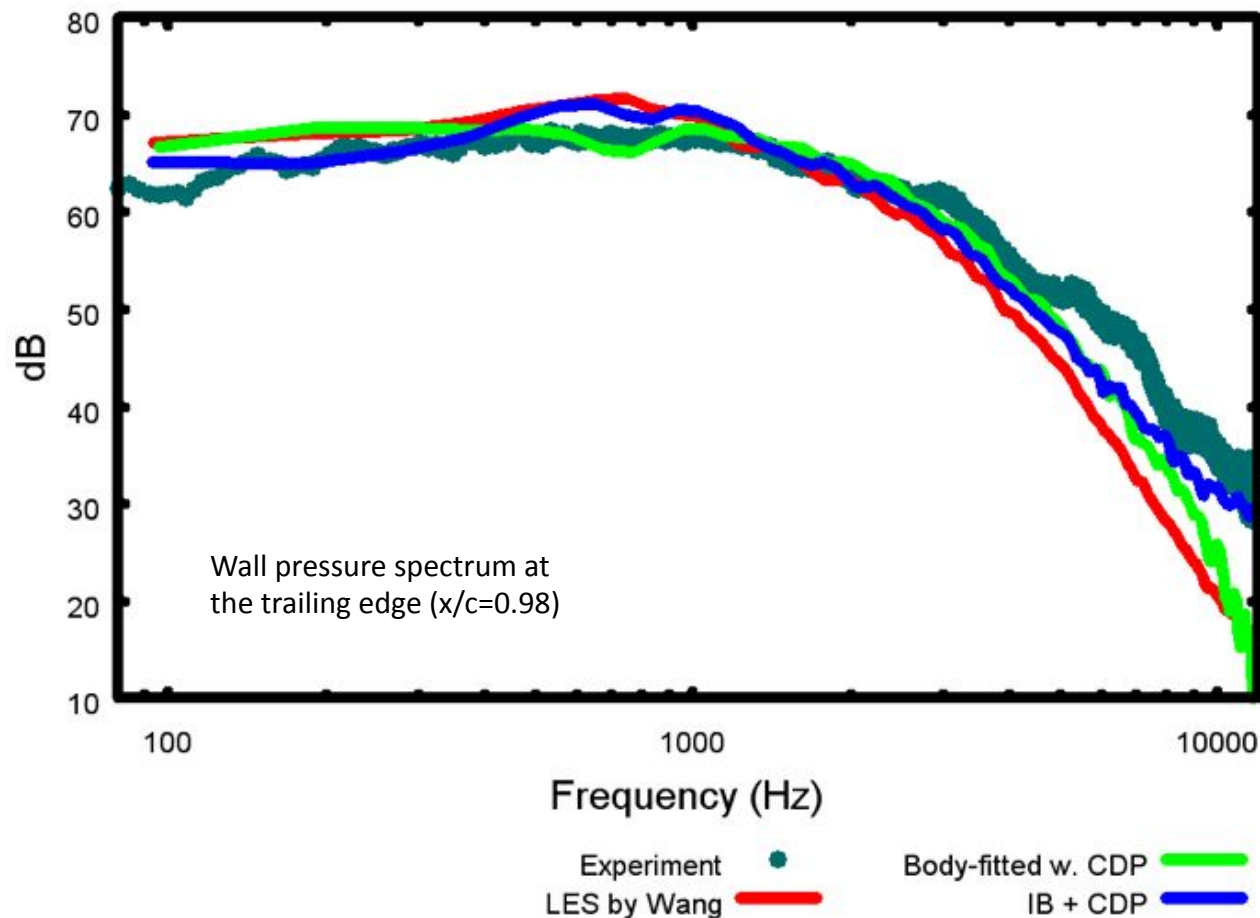
Downstream



Acoustic Predictions

Comparisons of velocity profiles in the wake and pressure distribution on the surface is very favorable

Much more challenging is the prediction of the wall pressure fluctuations

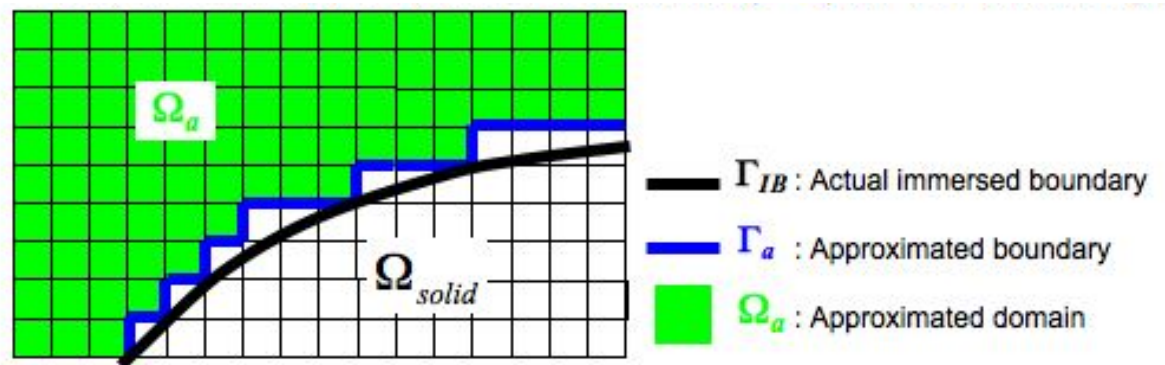


Summary

IB faces (ibwalls) are **always inside** the computational domain:
effectively the **reconstruction is always an interpolation**

Use of Locally Refined Grid creates additional complexity in the
reconstruction step

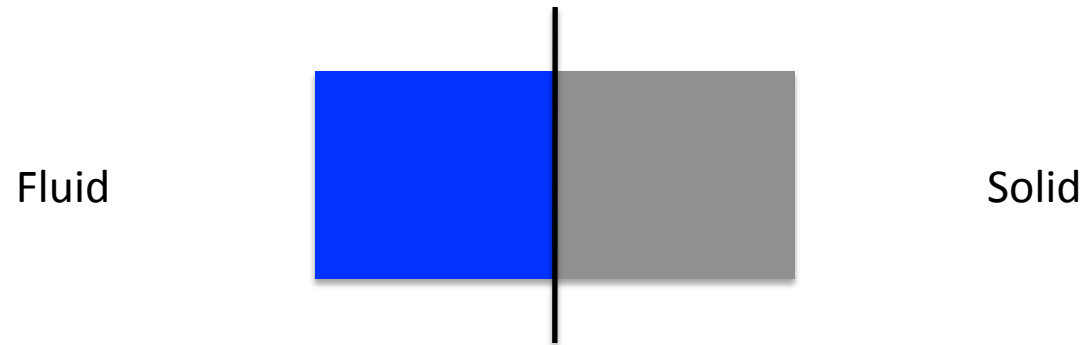
Enforcing mass conservation is NOT trivial but important and lead to
more accurate results!



5. Solid/Fluid Thermal Coupling

Solid/Fluid Thermal Coupling
Using the Immersed Boundary Method

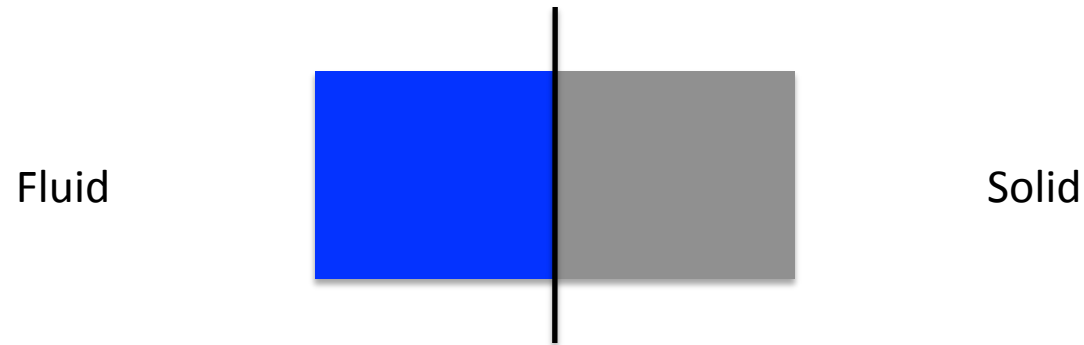
Multi-Domain Coupling



$$\frac{\partial \rho h}{\partial t} + \frac{\partial \rho u_j h}{\partial x_j} = \frac{\partial}{\partial x_j} \left[k \frac{\partial T}{\partial x_j} \right]$$

Because of discontinuities in physical properties (conductivity, etc) it is preferred to apply boundary conditions rather than differentiate across the interface!

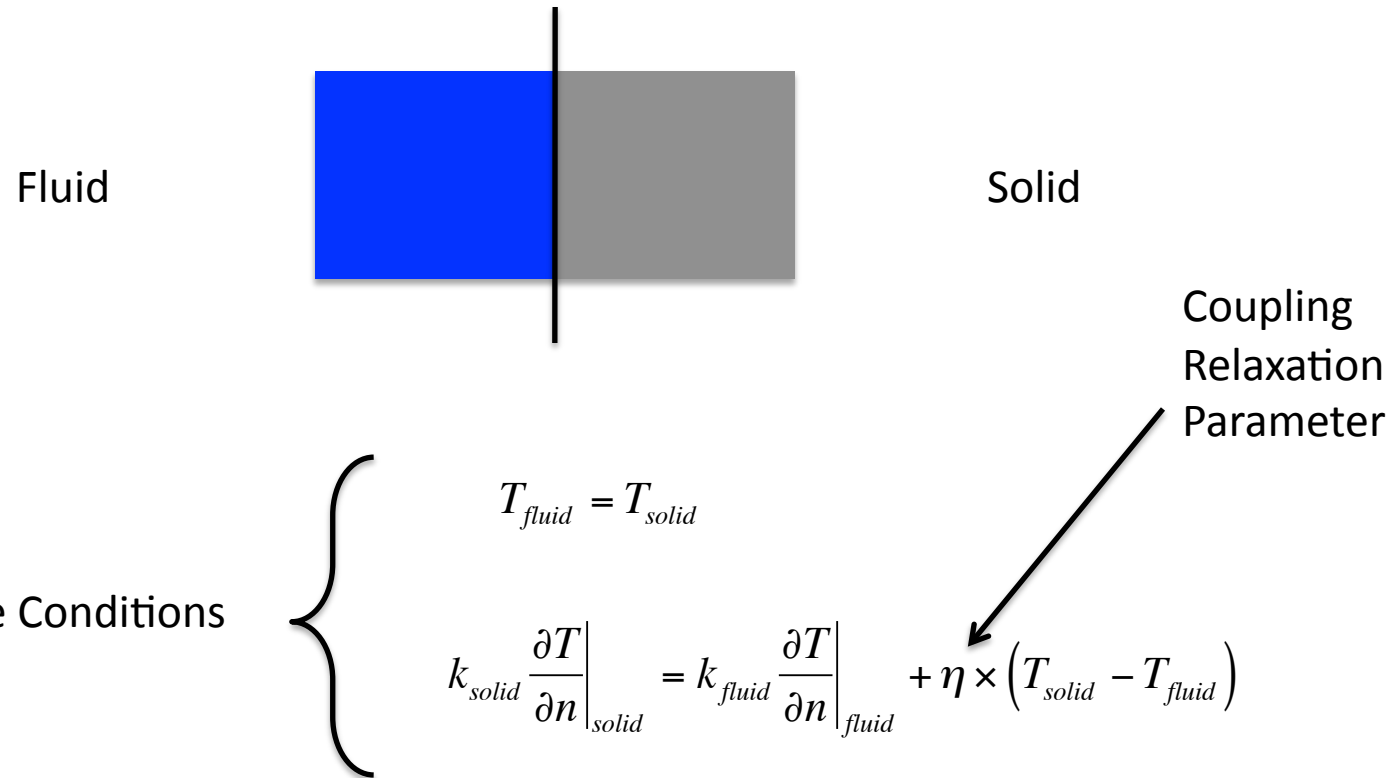
Multi-Domain Coupling



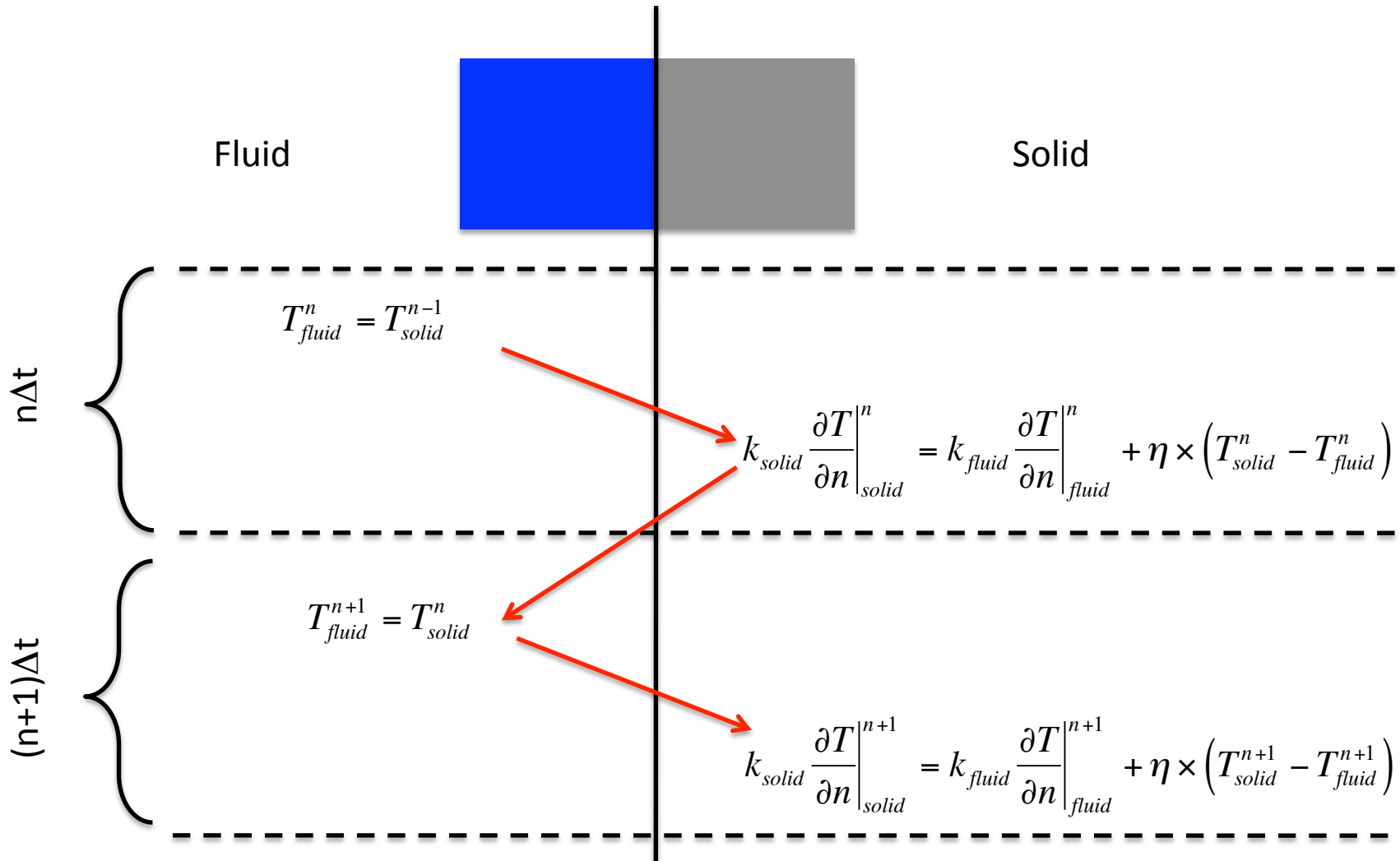
Interface Conditions

$$\left\{ \begin{array}{l} T_{fluid} = T_{solid} \\ k_{solid} \frac{\partial T}{\partial n} \Big|_{solid} = k_{fluid} \frac{\partial T}{\partial n} \Big|_{fluid} \end{array} \right.$$

Multi-Domain Coupling



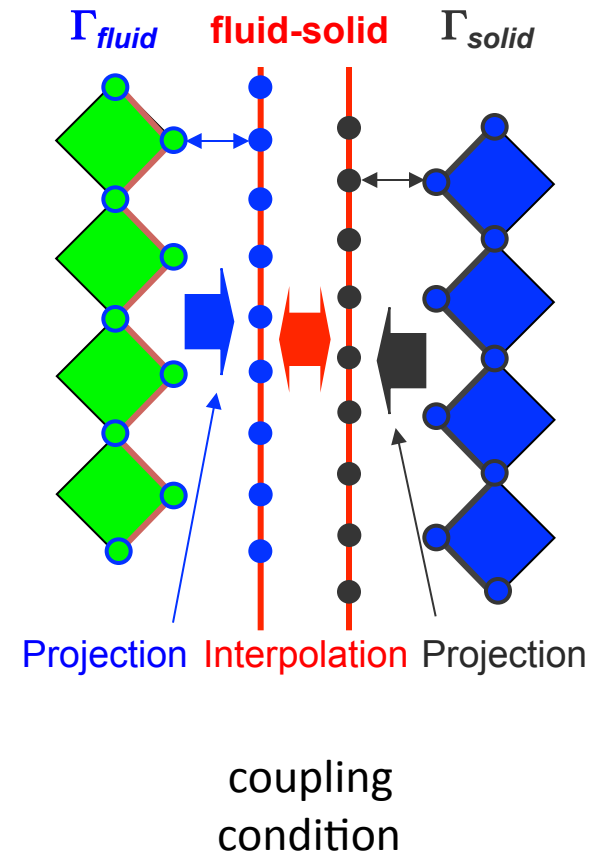
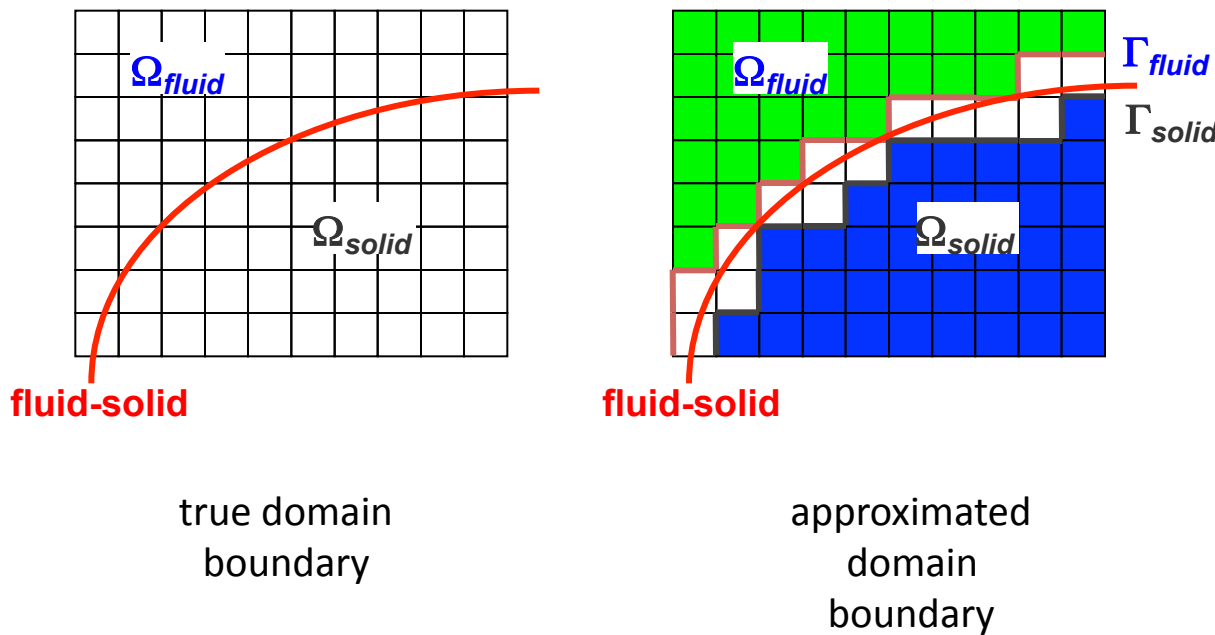
Multi-Domain Coupling



Staggered coupling procedure

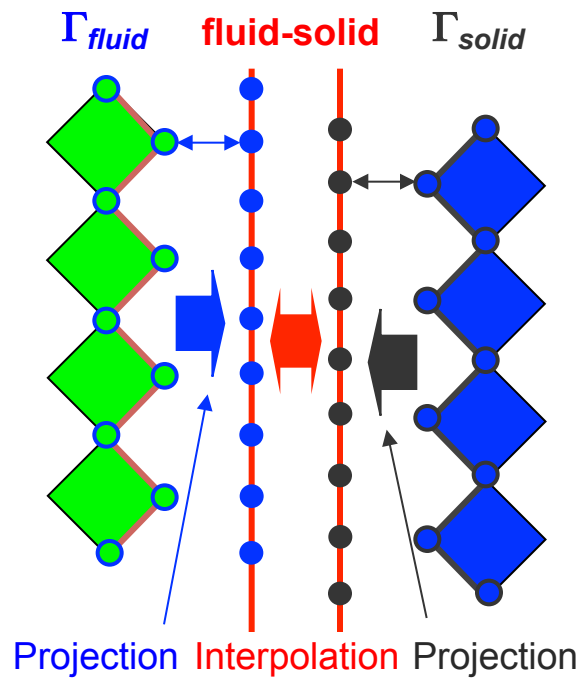
IB Multi-Domain Coupling

The energy equation is NOT solved across the subdomains, but boundary conditions are formally applied at the interface



We apply the IB reconstruction method on both sides of the interface

IB Multi-Domain Coupling



What is actually coupled?

Continuity of temperature

$$T_{fluid} = \overline{T_{solid}}$$

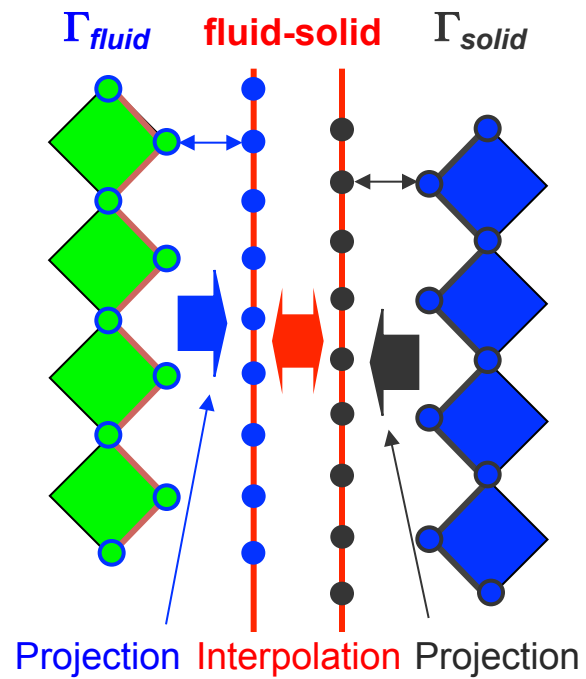
Continuity of heat flux

$$k_{solid} \left. \frac{\partial T}{\partial n} \right|_{solid} = \overline{k_{fluid} \left. \frac{\partial T}{\partial n} \right|_{fluid}}$$

Overbar indicates surface interpolation operators (on the “true” surface)

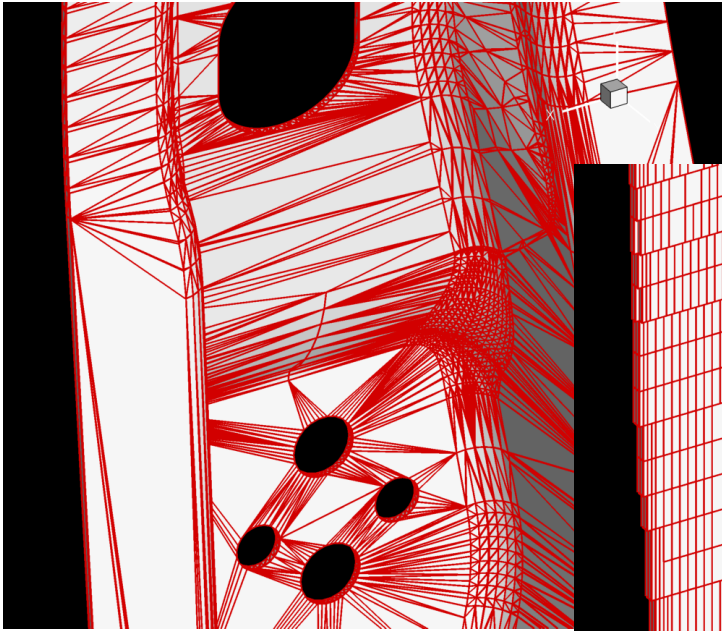
Asymmetric boundary condition enforcement

Interface Interpolation

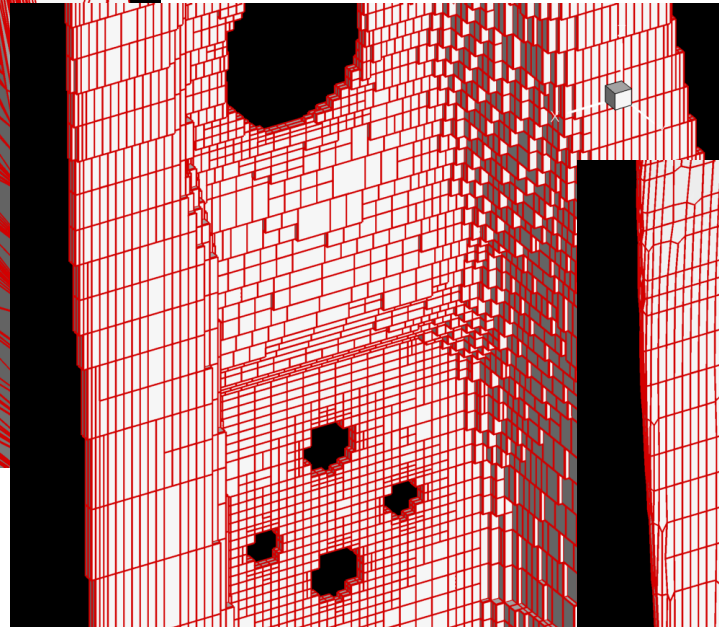


We need the actual interface geometry....

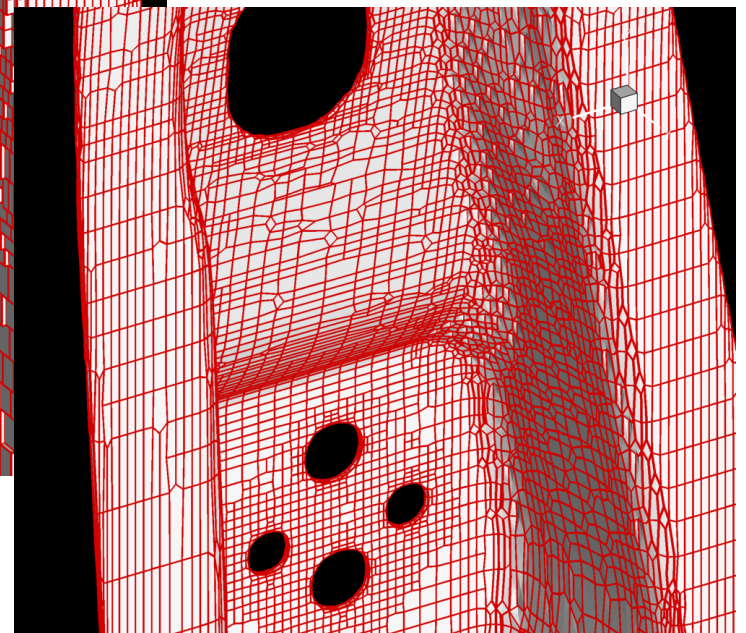
Interface Grid Reconstruction



original stl

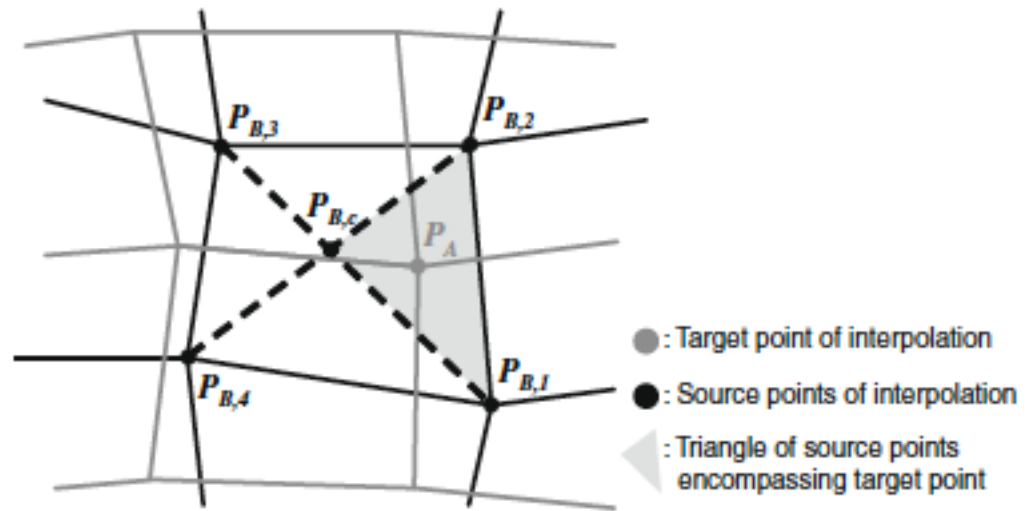
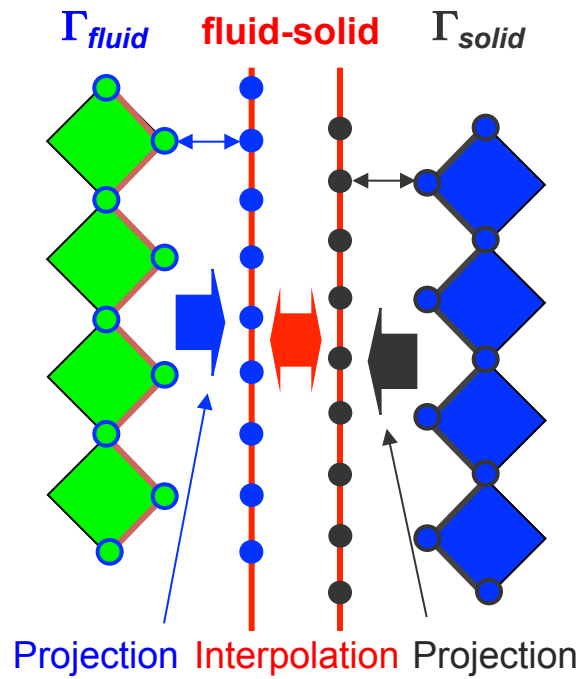


stairstep tommye
grid



projected tommye
grid

Interface Interpolation



Validation Test, I

Flow generated by a heated sphere

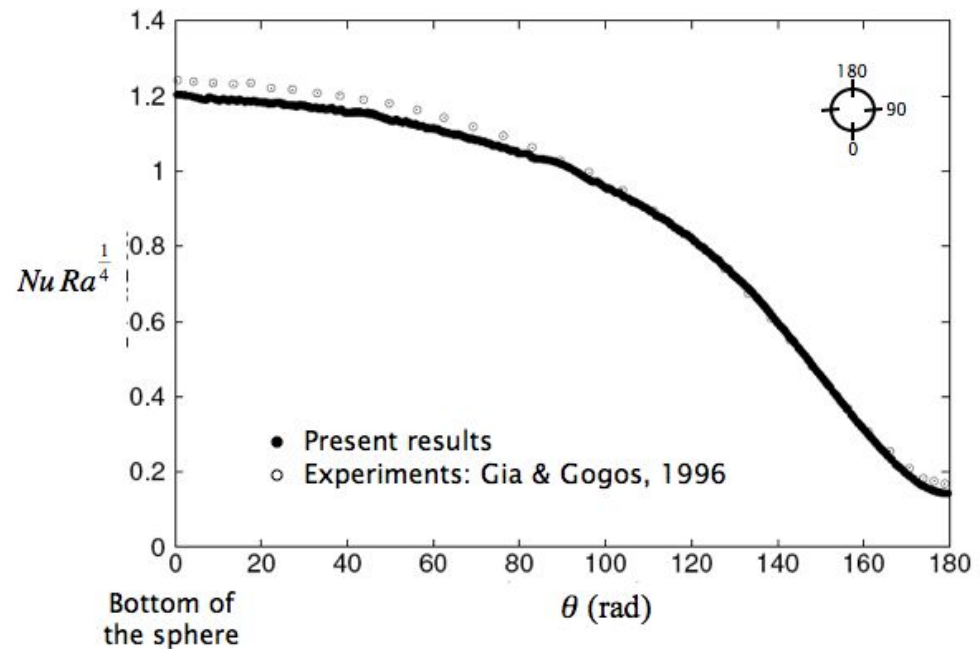
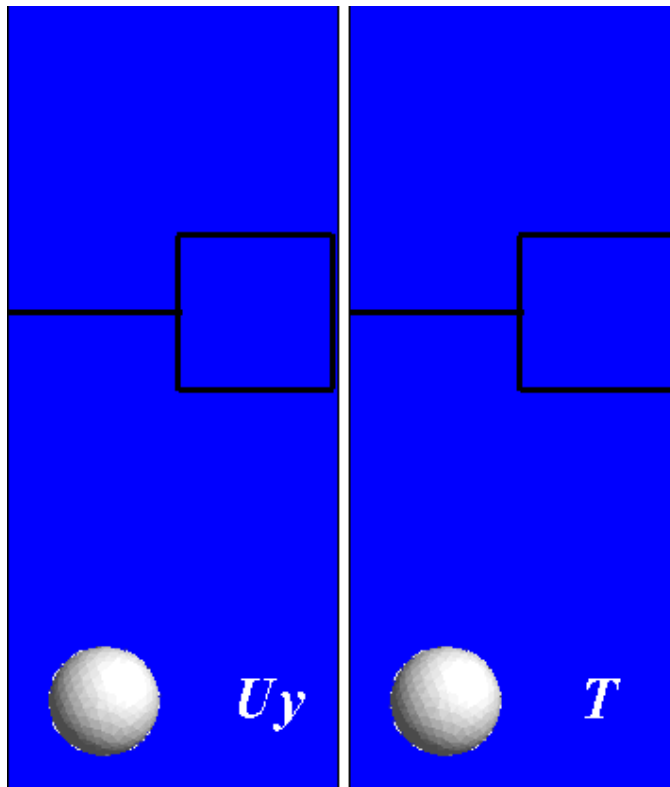
$$Gr = 10^4$$

Constant temperature on the sphere

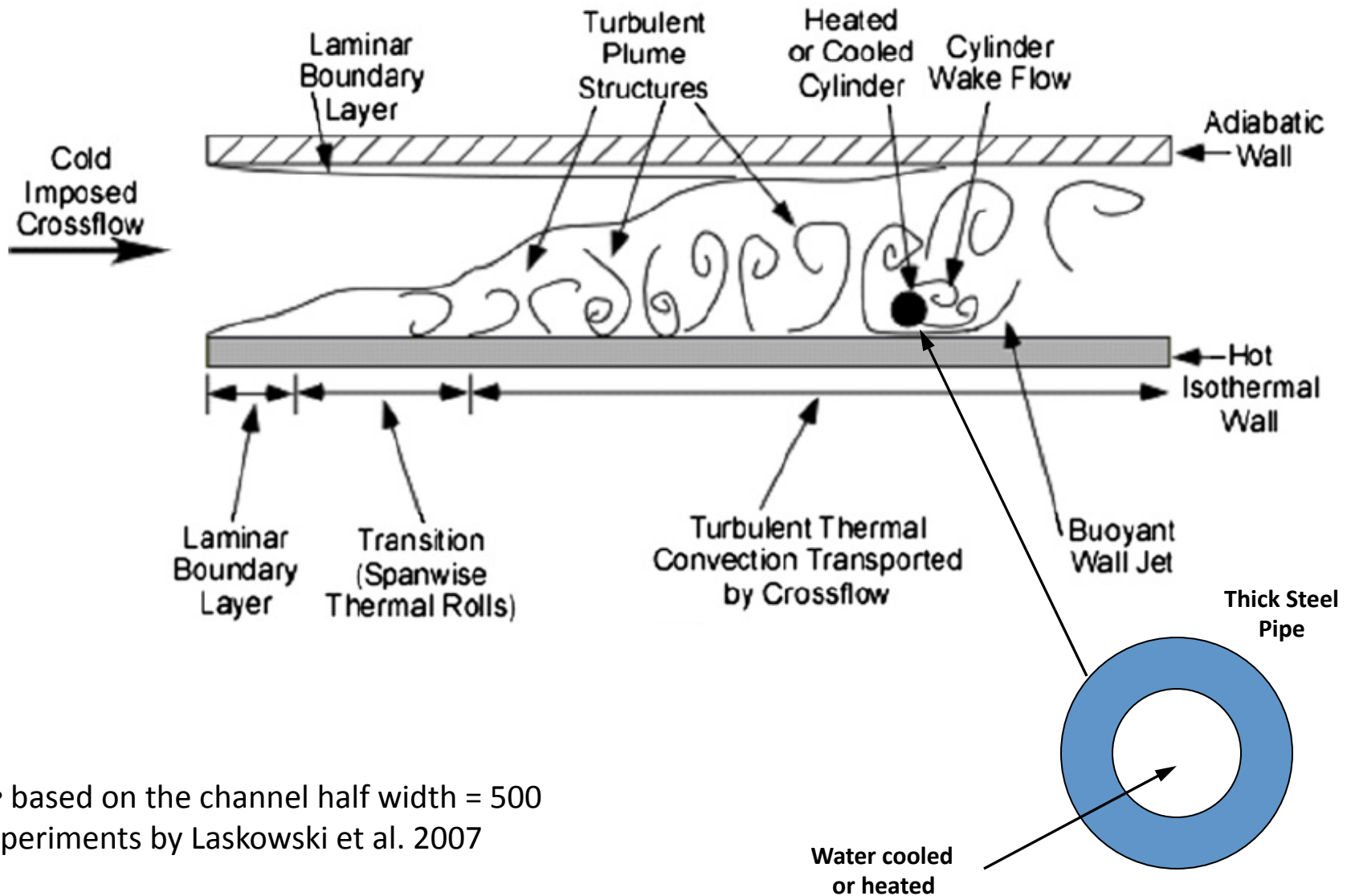
Natural convection, Boussinesq approximation

Mesh:

~2.2M elements

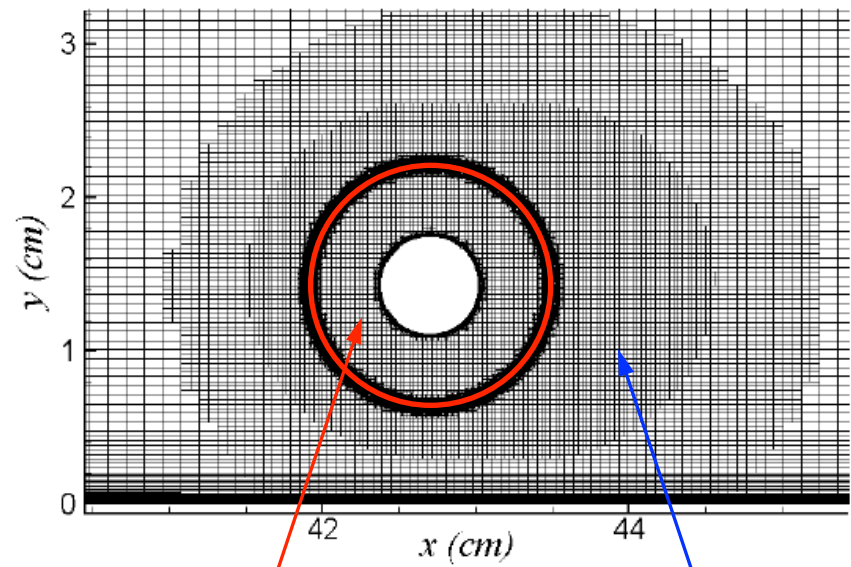
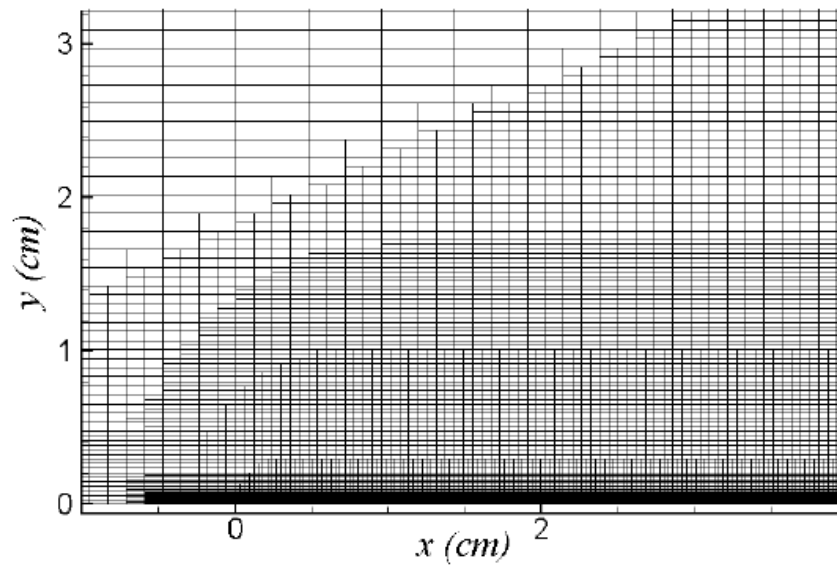
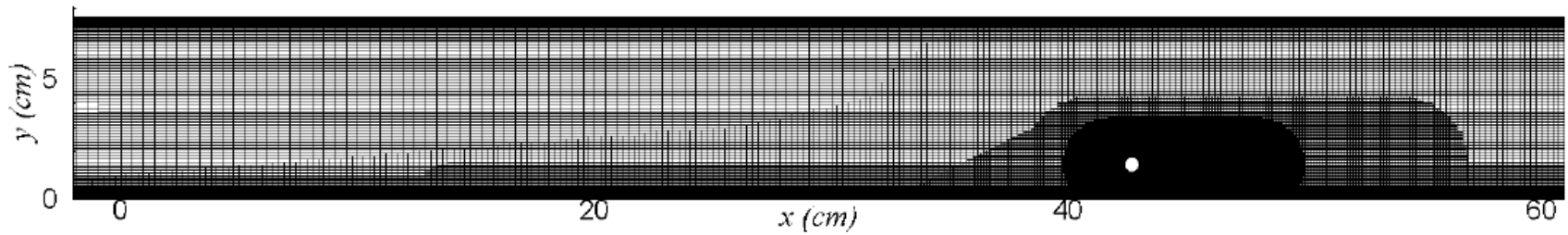


Validation Test, II



Re based on the channel half width = 500
Experiments by Laskowski et al. 2007

Computational Mesh



solid

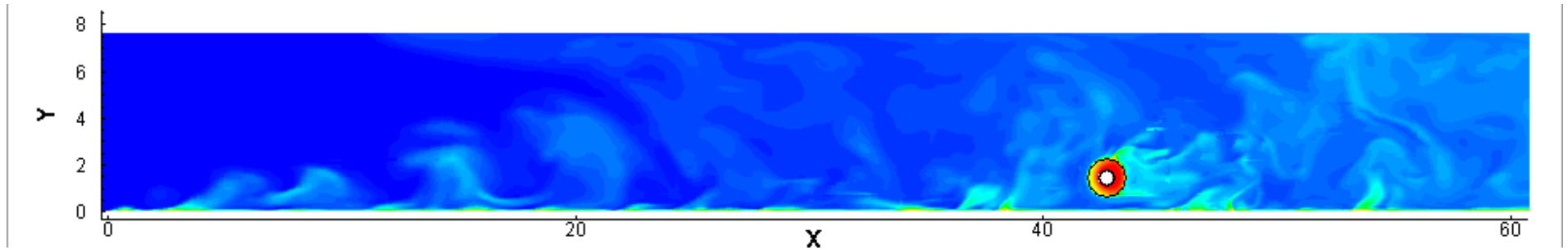
fluid

Grid size: 5-12M elements

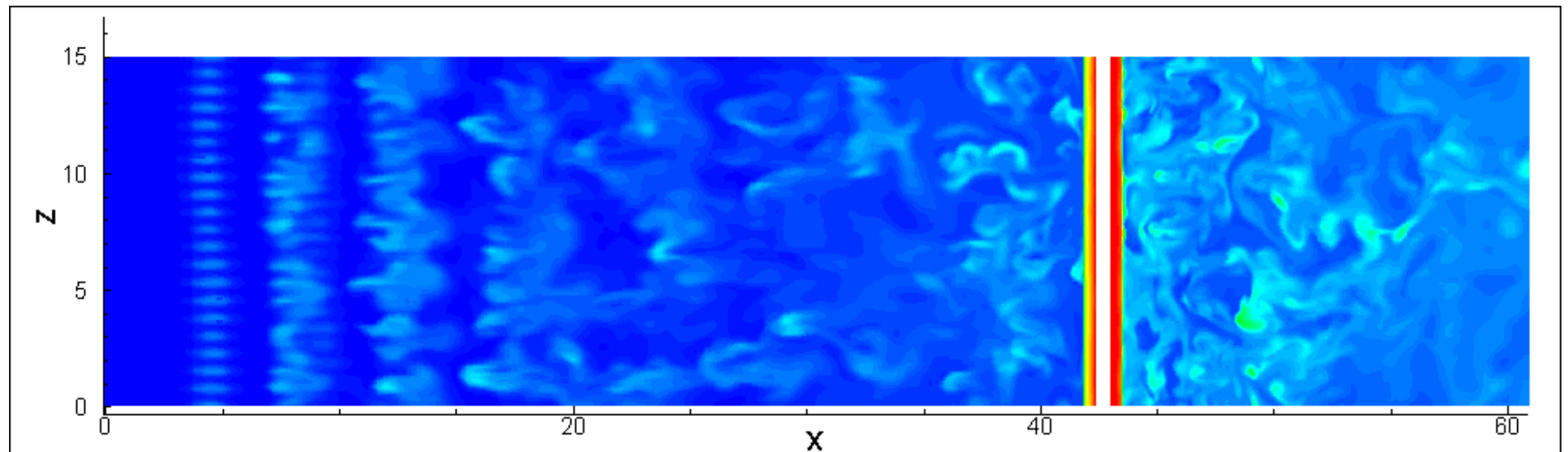
Simulation Results

Temperature field

Side view

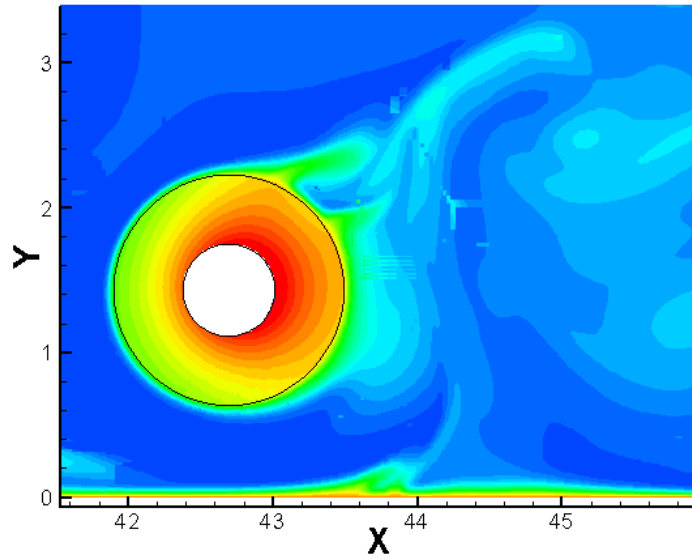


Top view



Heating starts at $x=0$ on the bottom plate. The BL is thermally unstable...

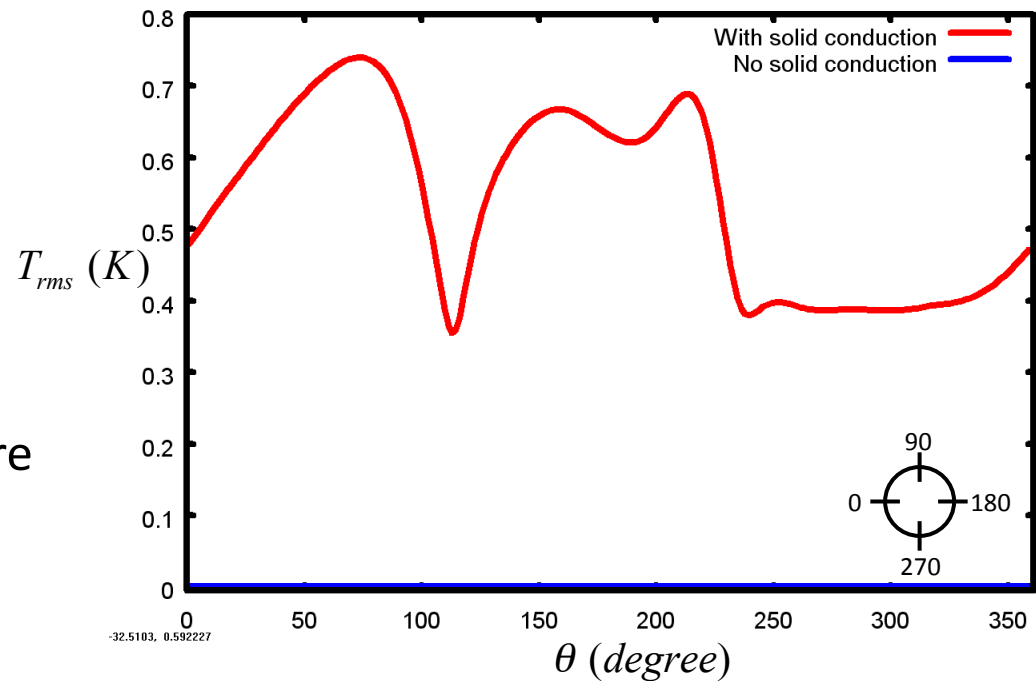
The Effect of Solid Conduction



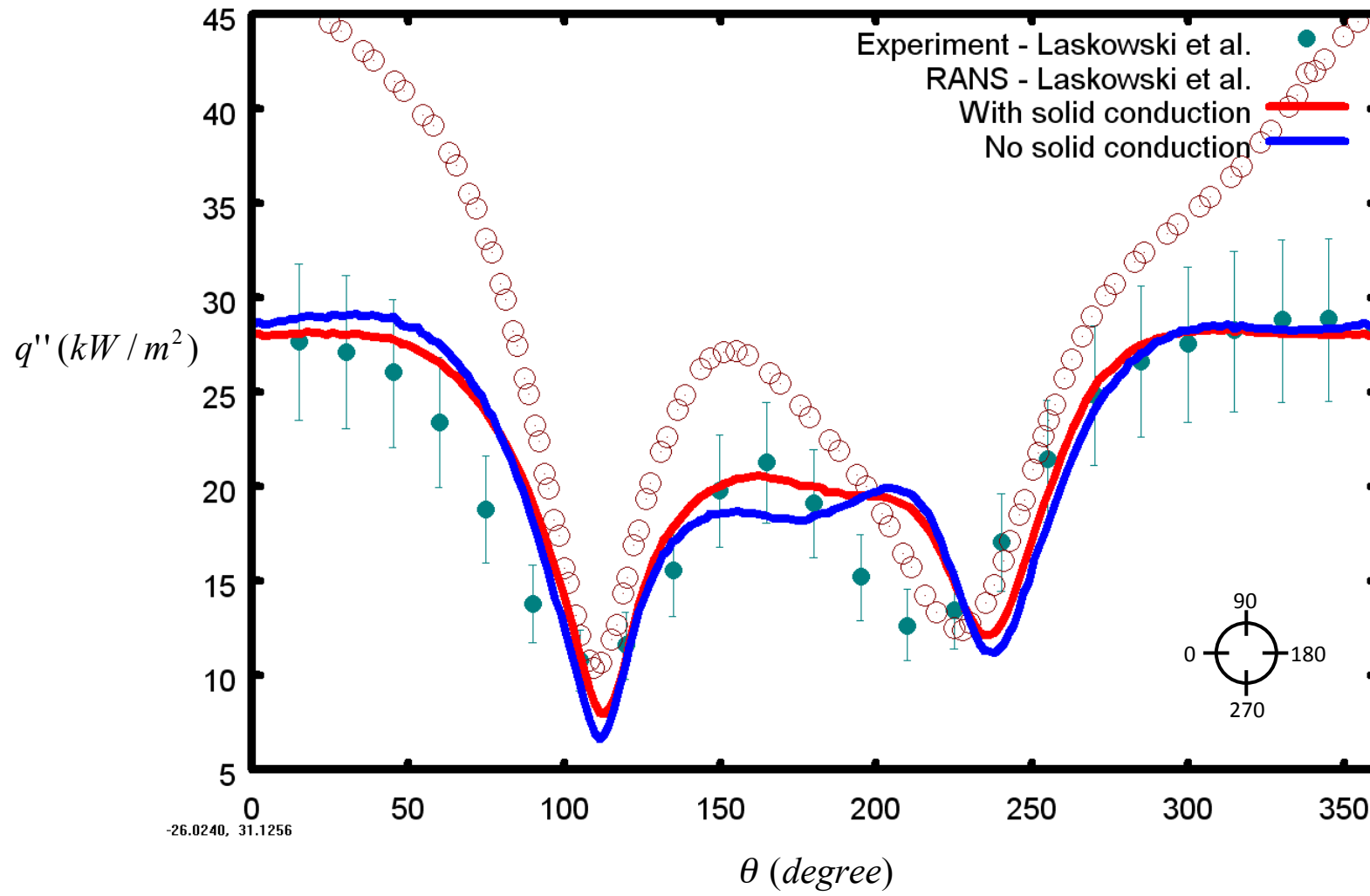
Highly unsteady turbulent flow field in the wake result in motion of the separation points on the cylinder

Thermal plumes from the upstream BL hit the cylinder at the stagnation point

As a result the wall temperature is NOT stationary

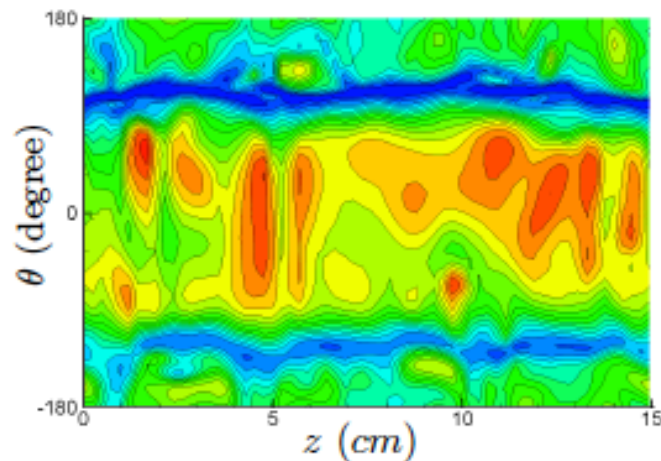


The Effect of Solid Conduction

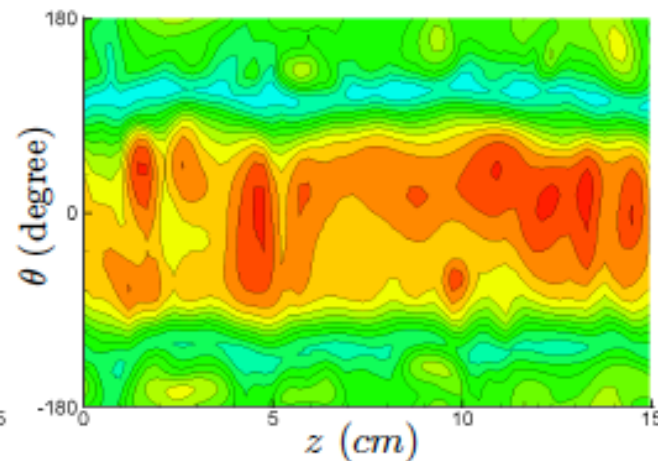


-26.0240, 31.1256

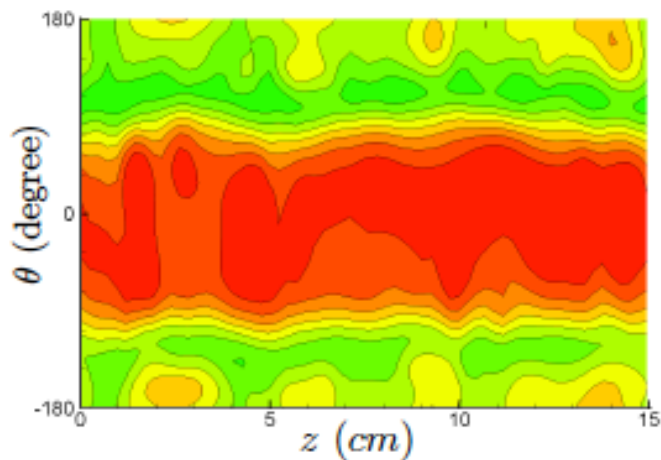
Instantaneous Temperature Field



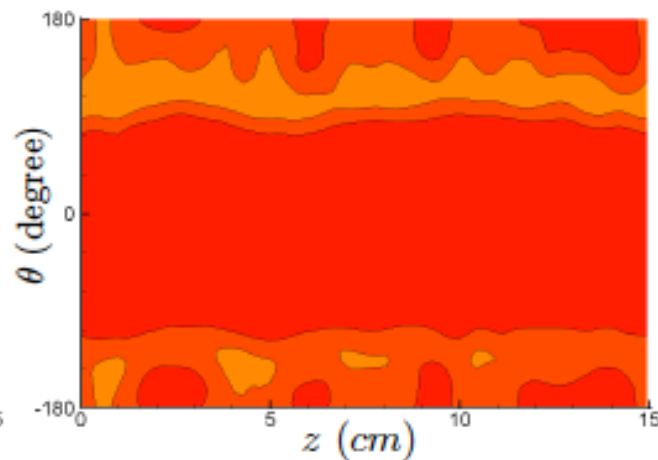
(a) At the outer cylinder ($r=0.79\text{cm}$)



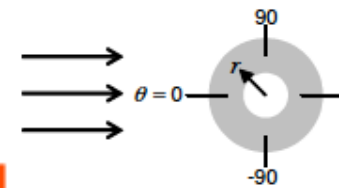
(b) At $r=0.68\text{cm}$



(c) At $r=0.57\text{cm}$



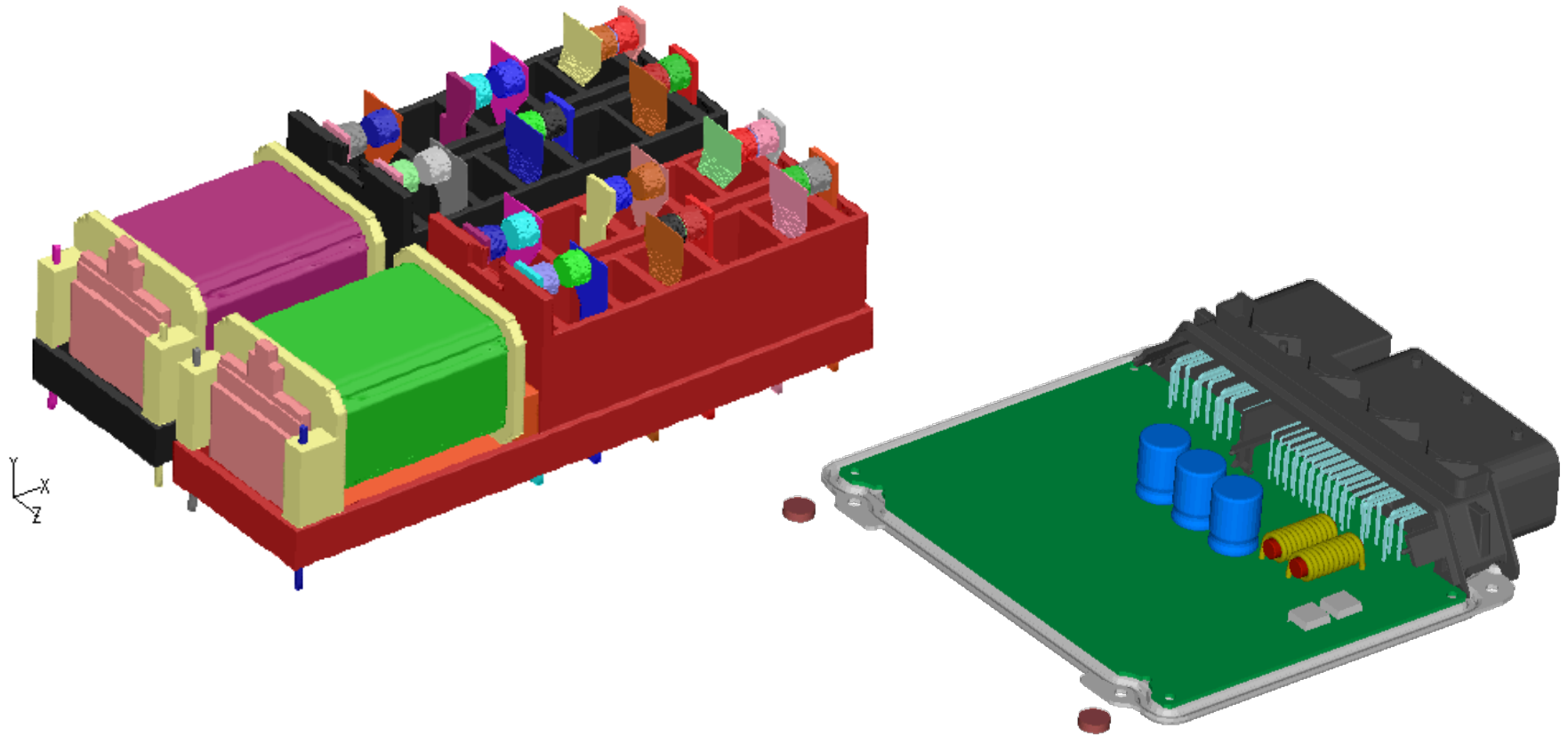
(d) At $r=0.47\text{cm}$



6. Applications

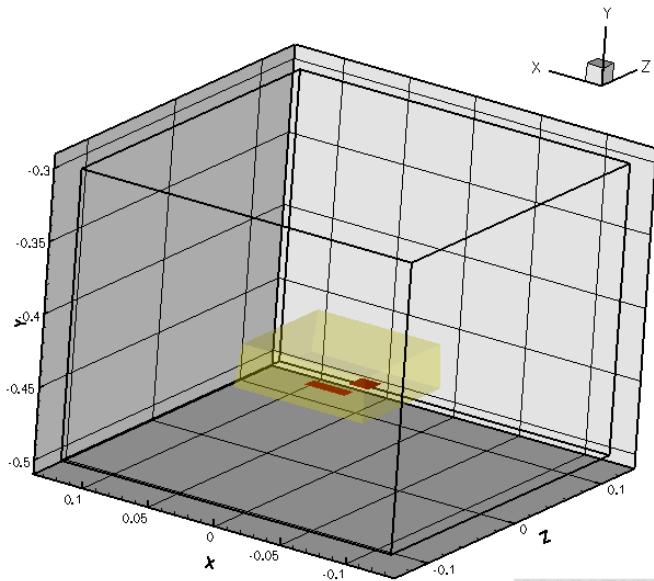
Solid/Fluid Thermal Coupling
Using the Immersed Boundary Method

Electronic Component Units



Electronic Components

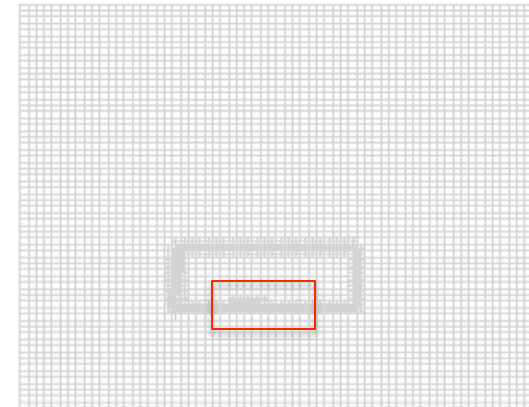
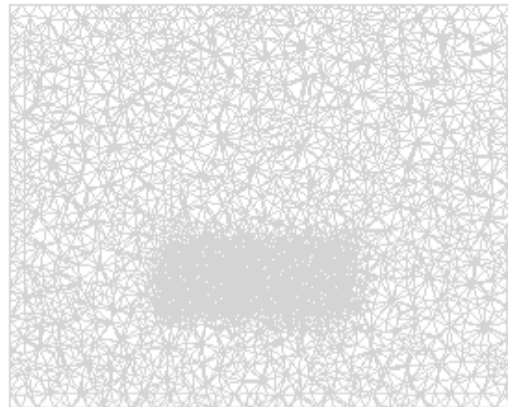
A simple test case: Conduction + Natural Convection



2 Hot Spots (CPUs)
1 Plastic Mold
in a air-filled cavity

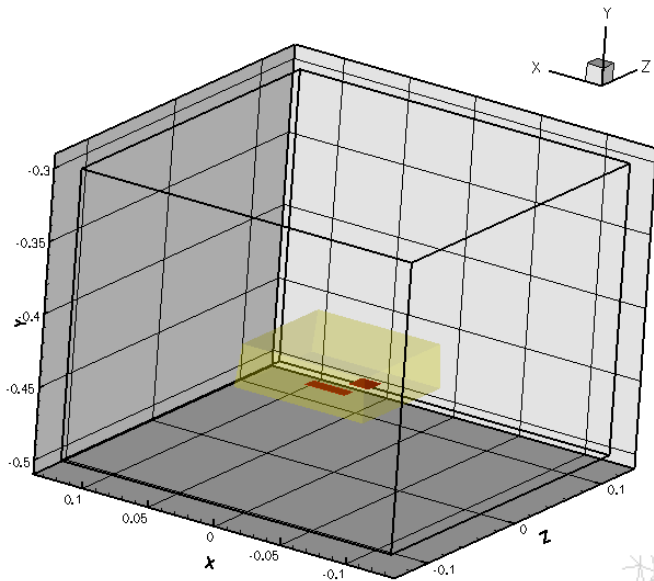
Body-Fitted
420K Cells

IB
380K Cells



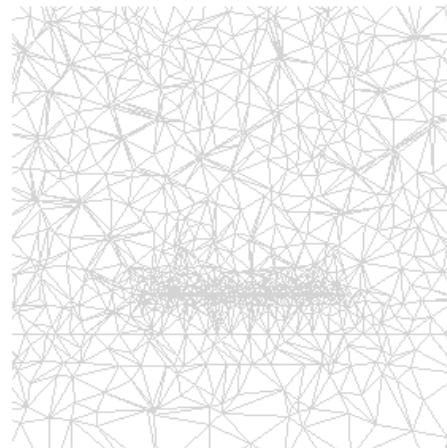
Electronic Components

A simple test case: Conduction + Natural Convection

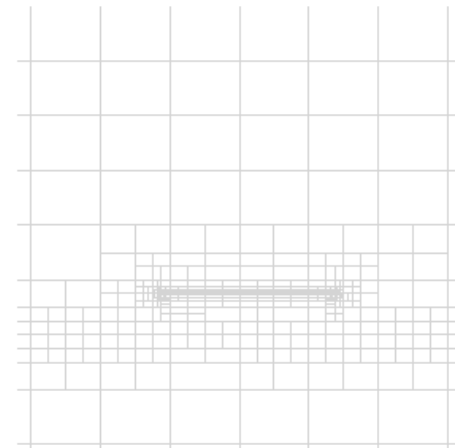


2 Hot Spots (CPUs)
1 Plastic Mold
in a air-filled cavity

Body-Fitted
420K Cells

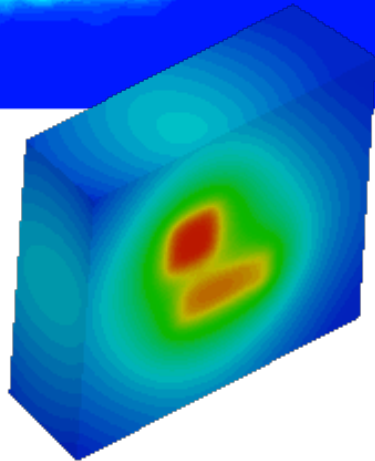
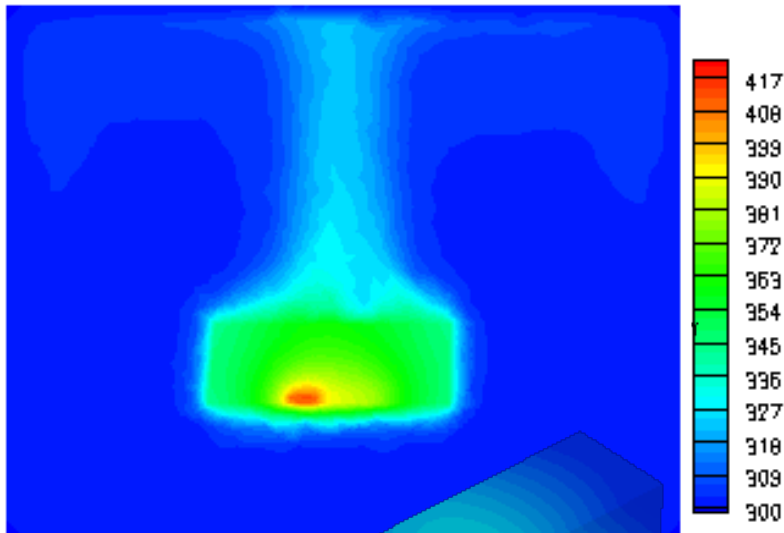


IB
380K Cells

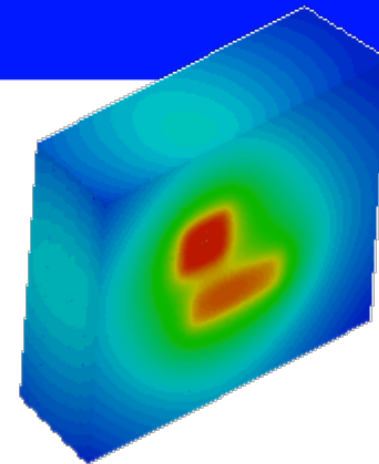
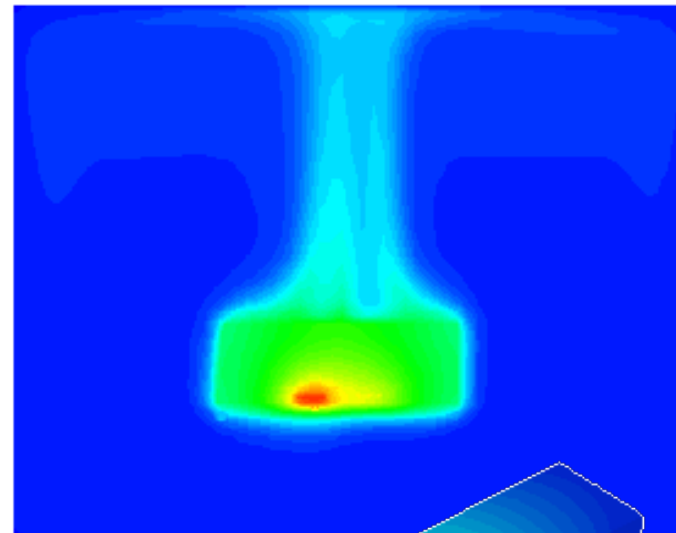


Temperature Field

Body Fitted

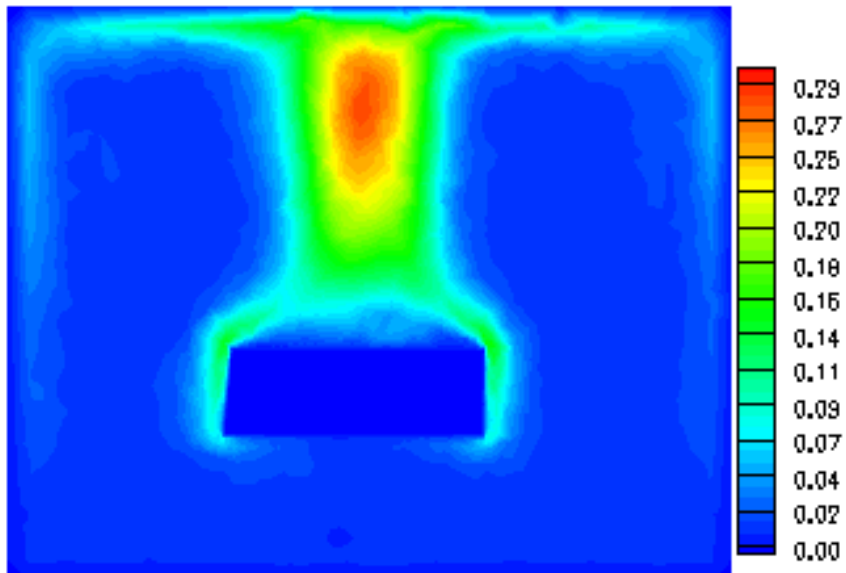


Immersed Boundary

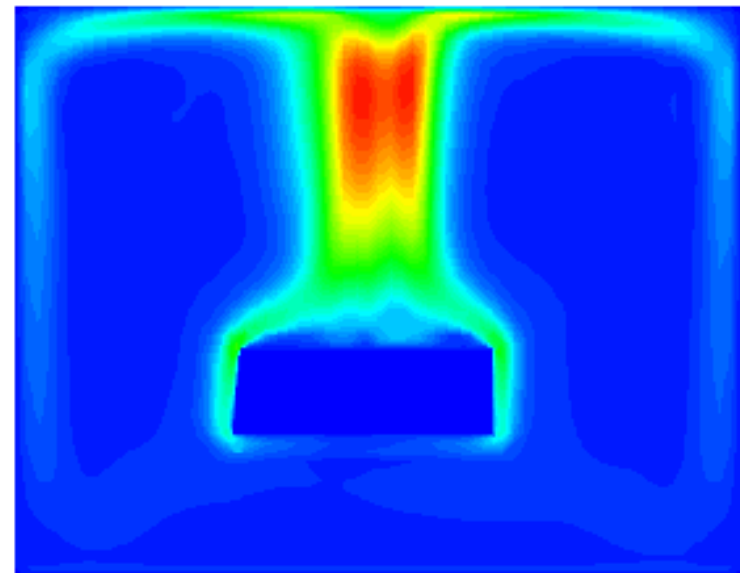


Velocity Field

Body Fitted

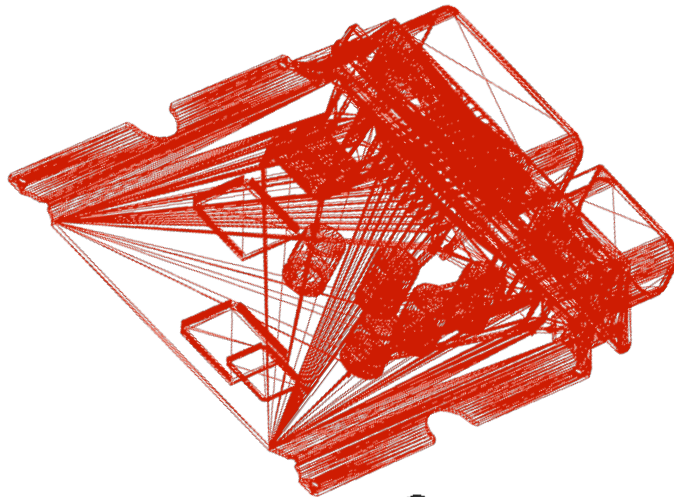


Immersed Boundary



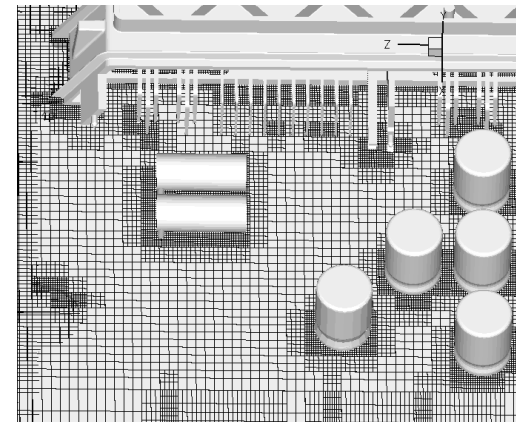
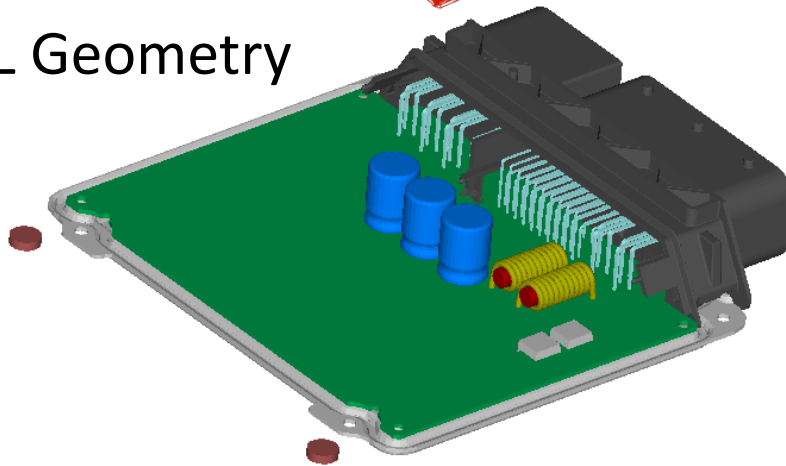
Electronic Component Unit

A complex test case: Conduction + Forced Convection



- Cartesian mesh
 - ~ 5.2 million cells
- Mesh contains ~ 10 solid zones for calculating conjugate heat transfer

STL Geometry



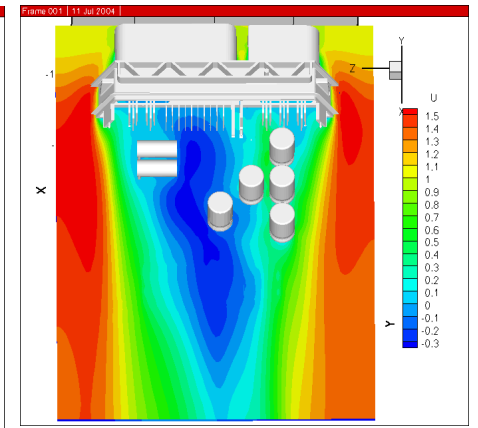
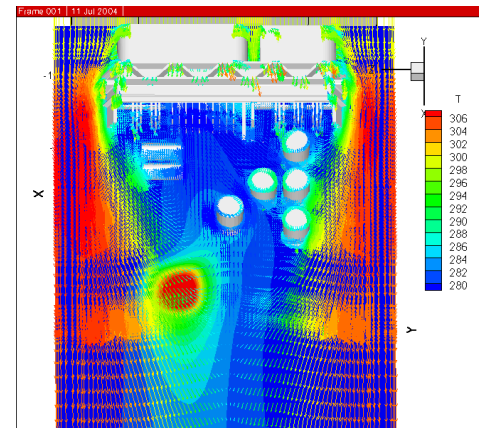
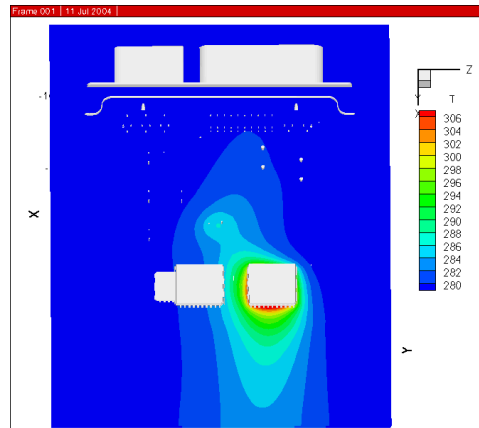
Electronic Component Unit

T_{top}

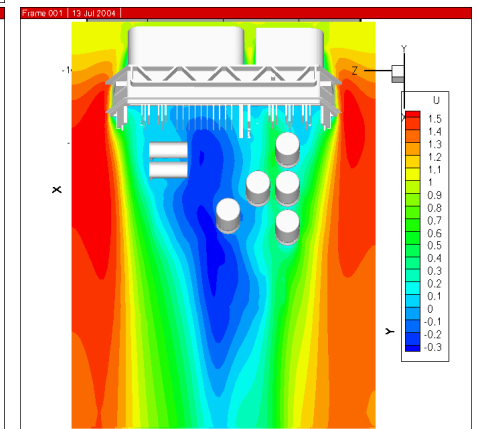
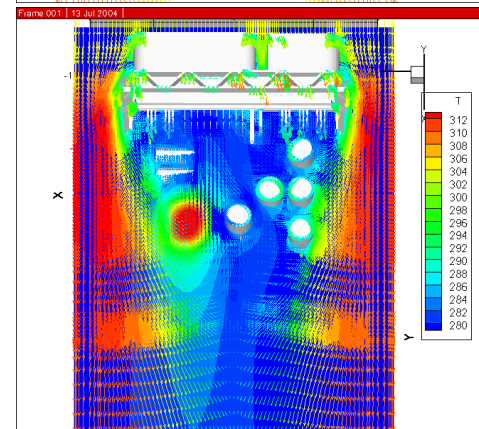
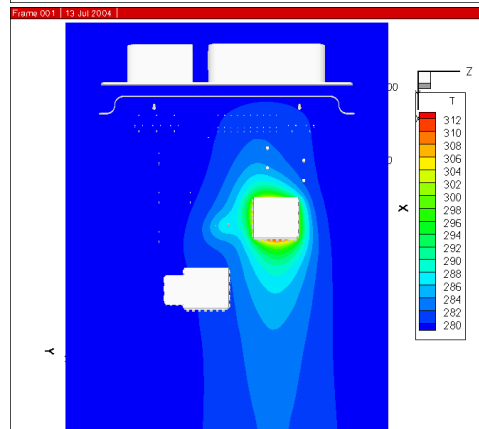
T_{bottom}

Velocity

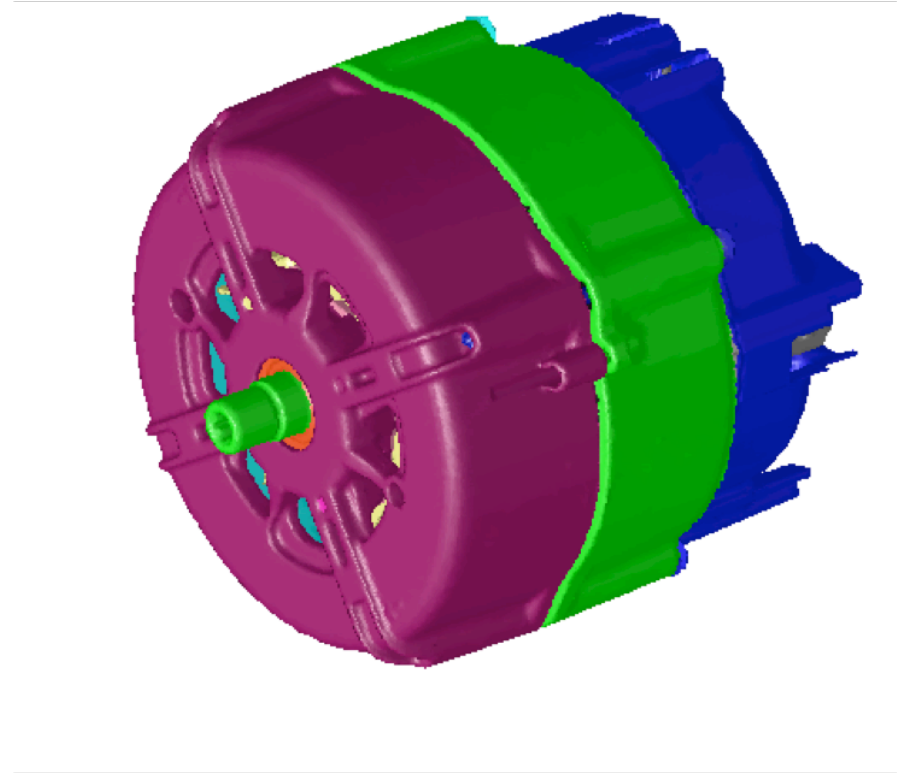
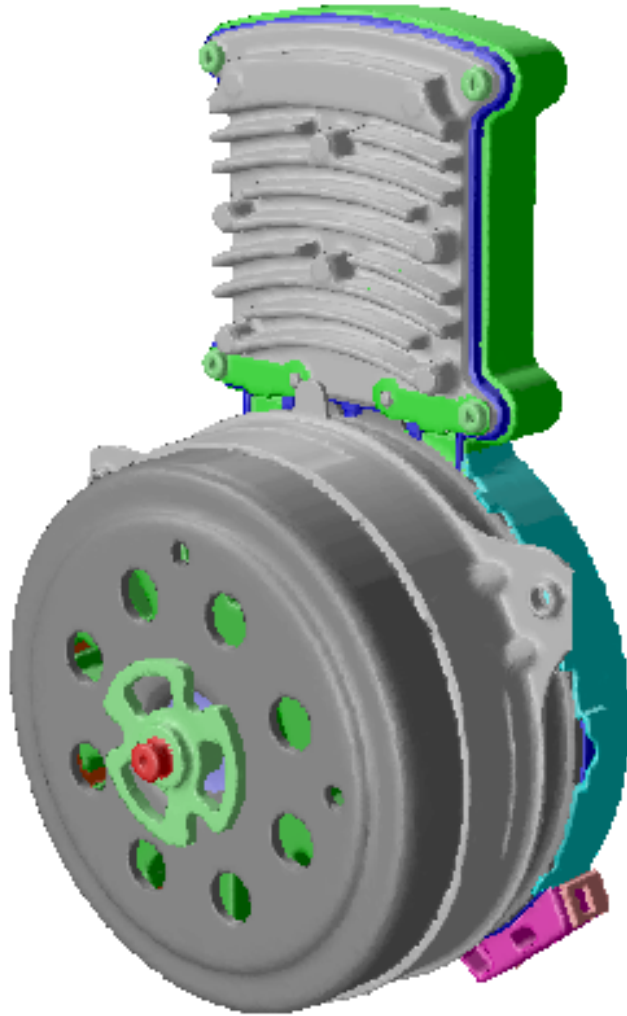
CASE 1:
 $T_{\text{max}} = 322 \text{ K}$



CASE 2:
 $T_{\text{max}} = 325 \text{ K}$



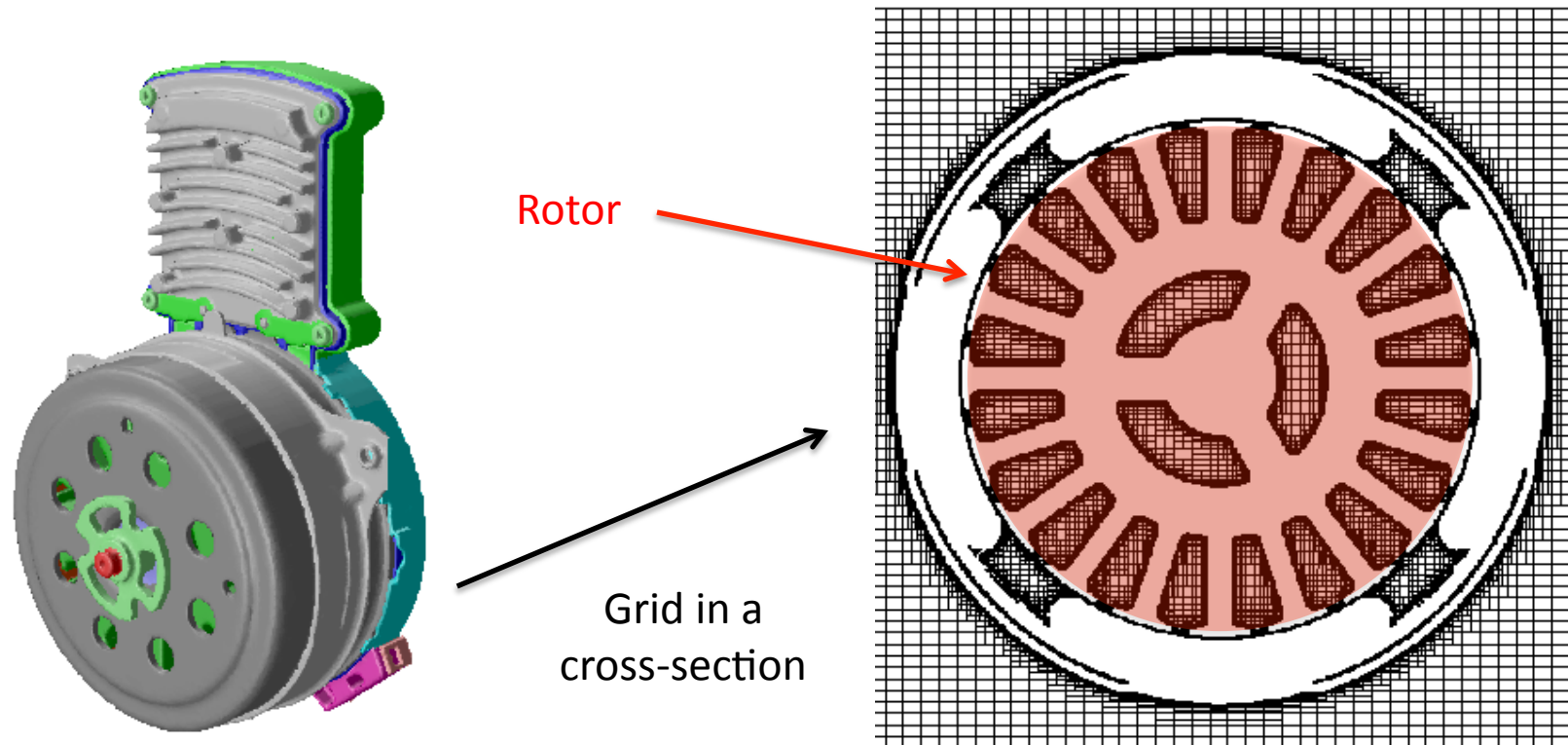
Electric Motors



The “world” is NOT Cartesian

Many of the industrial applications have moving/rotating parts and Cartesian grids are not ideal

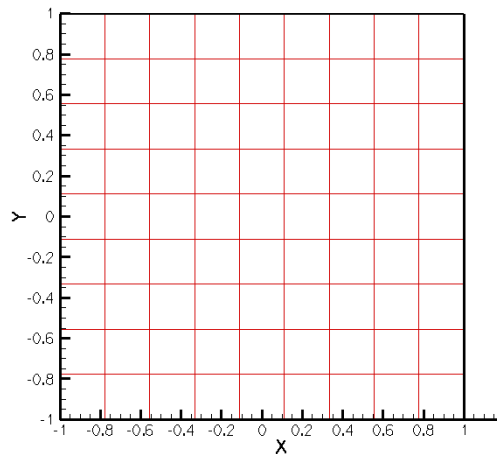
Example: Valeo Electric Motor



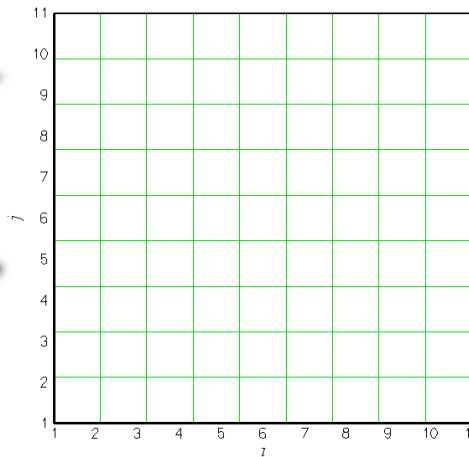
Beyond Cartesian Grids

The grids are not generated in the Physical Space but in a notional, integer space

- Addition of cells, and geometrical info are fast
- Tri-segment intersections are “exact”



Physical Space
(Real X Real)

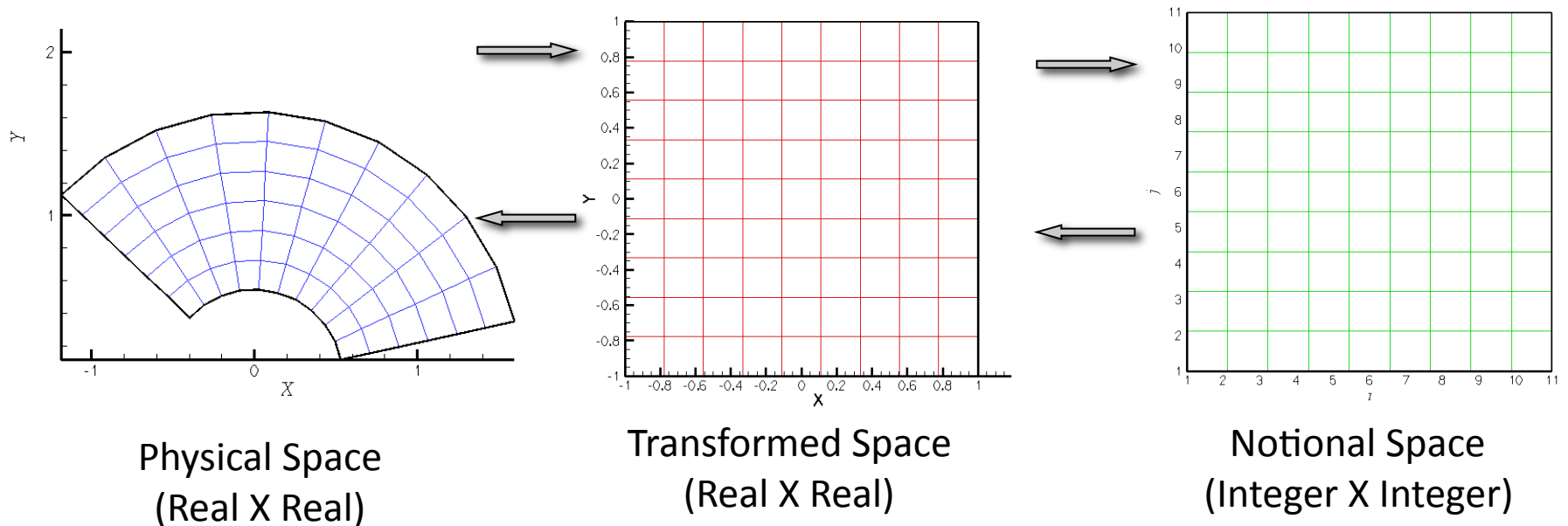


Notional Space
(Integer X Integer)

Beyond Cartesian Grids

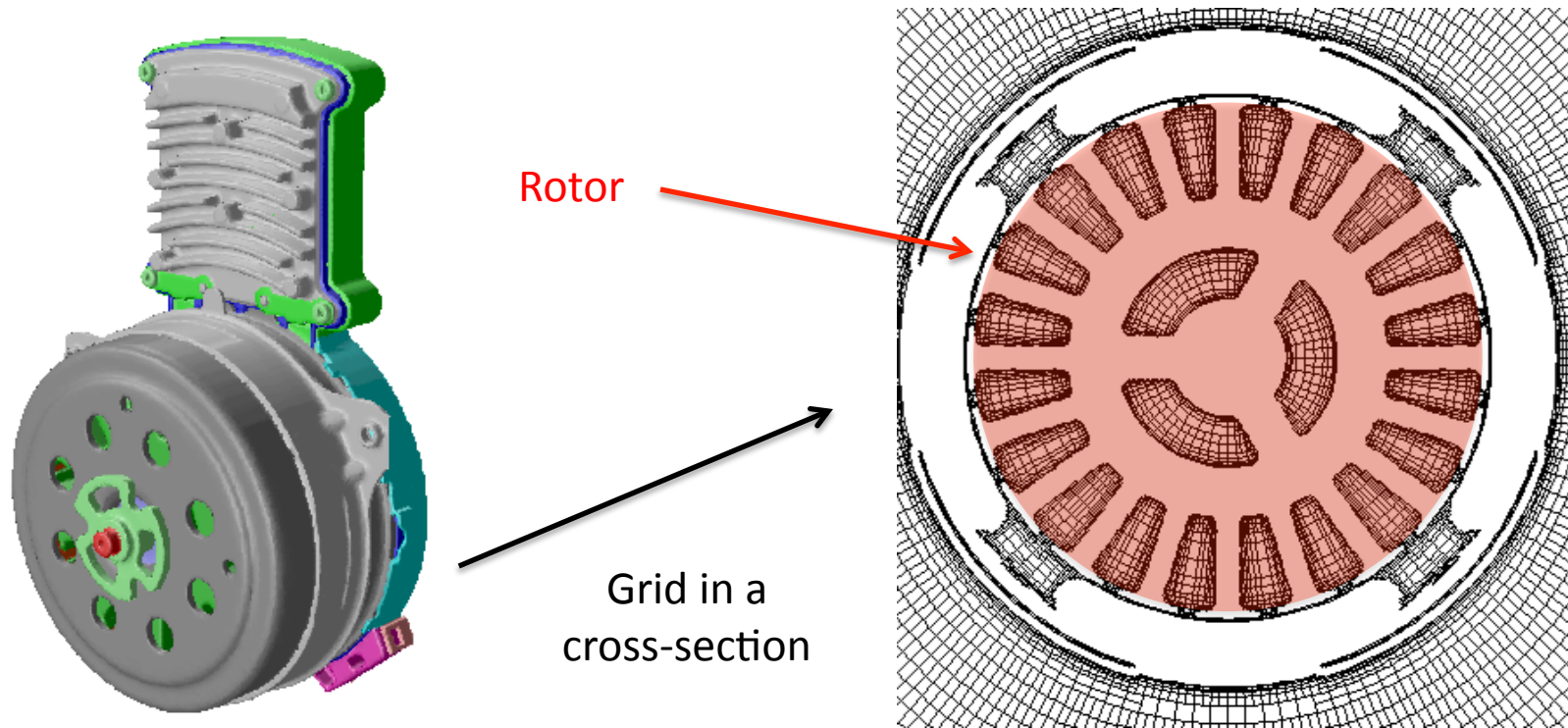
A coordinate transformation can be applied to the entire process

- Cylindrical-to-Cartesian
- Any generic invertible transformation

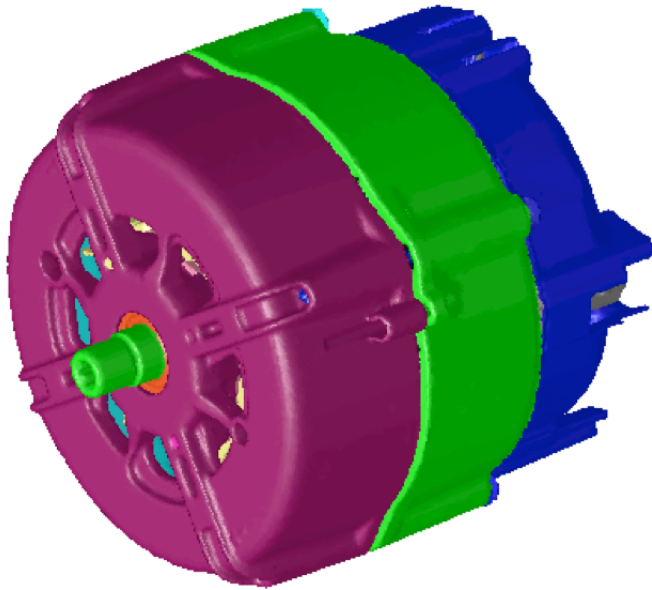


From Cartesian to Cylindrical

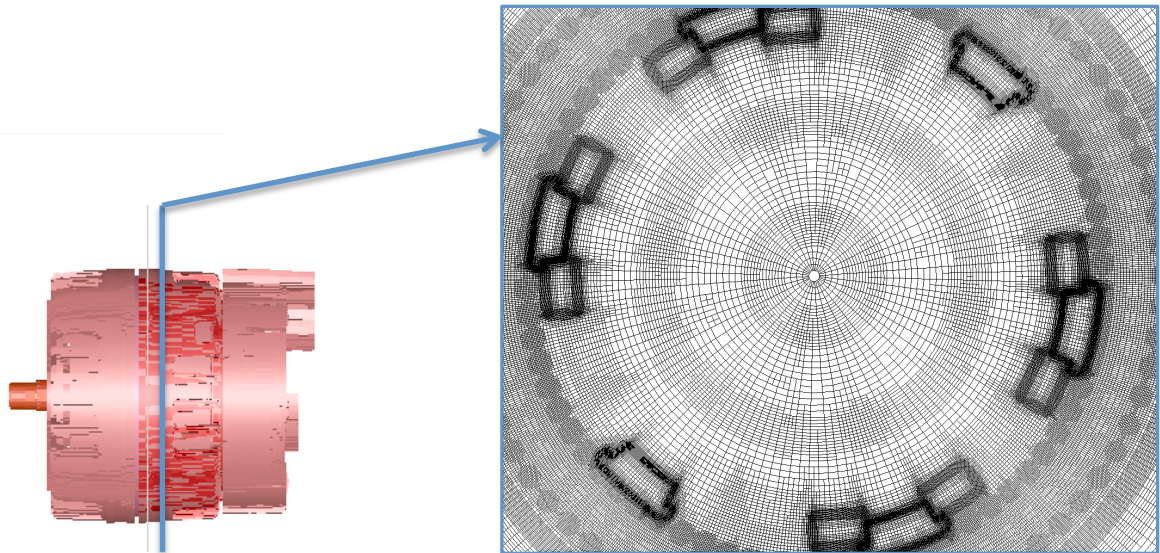
Example: Valeo Electric Motor



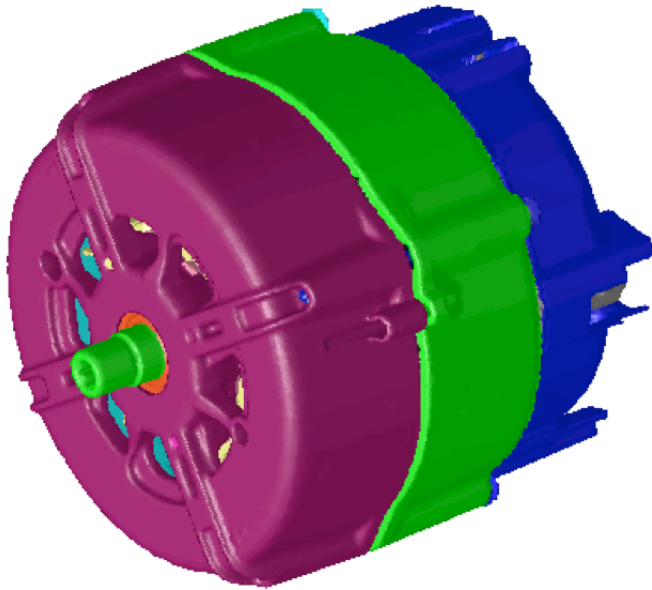
Alternator



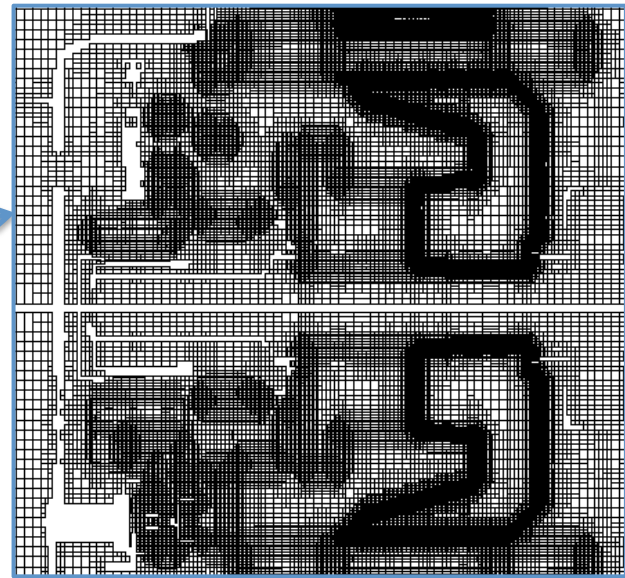
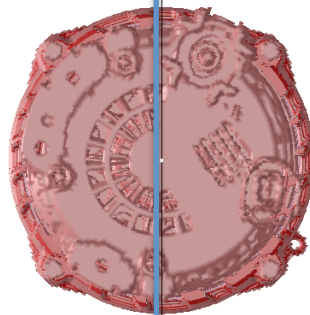
- Cylindrical mesh
 - ~ 16.2 million cells
- Mesh contains ~40 solid zones for calculating conjugate heat transfer



Alternator

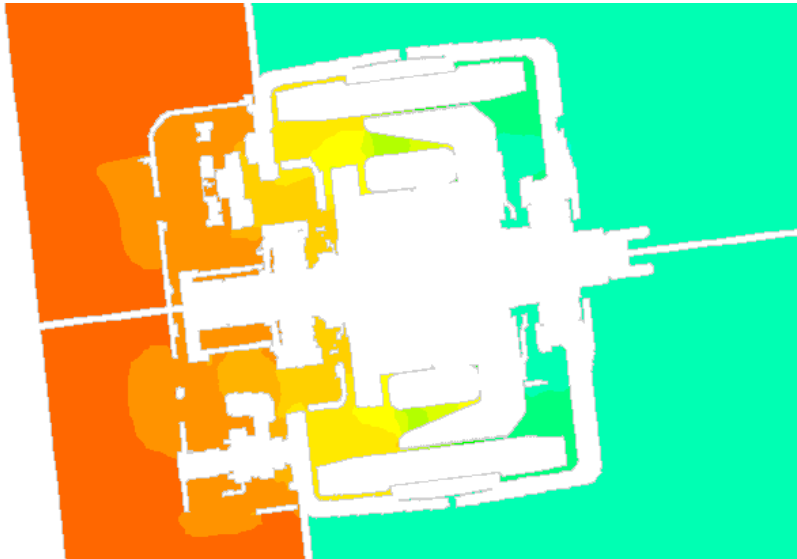


- Cylindrical mesh
 - ~ 16.2 million cells
- Mesh contains ~40 solid zones for calculating conjugate heat transfer

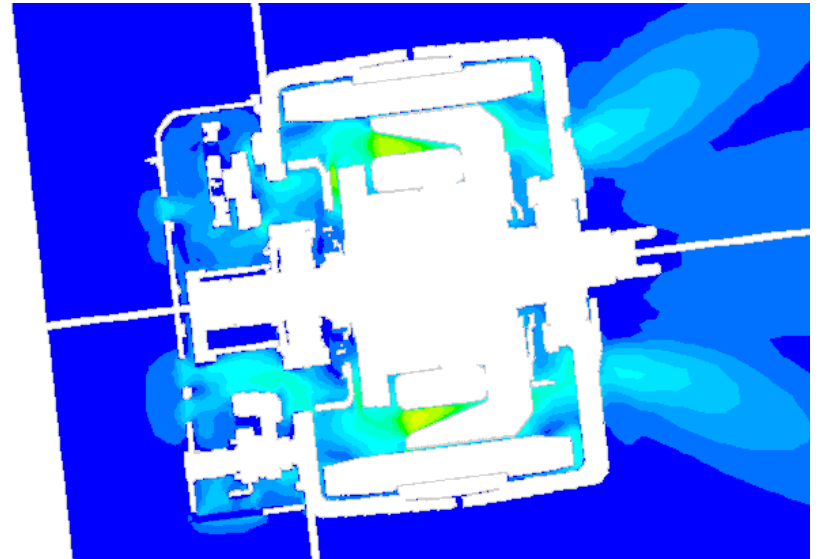


Alternator

Pressure

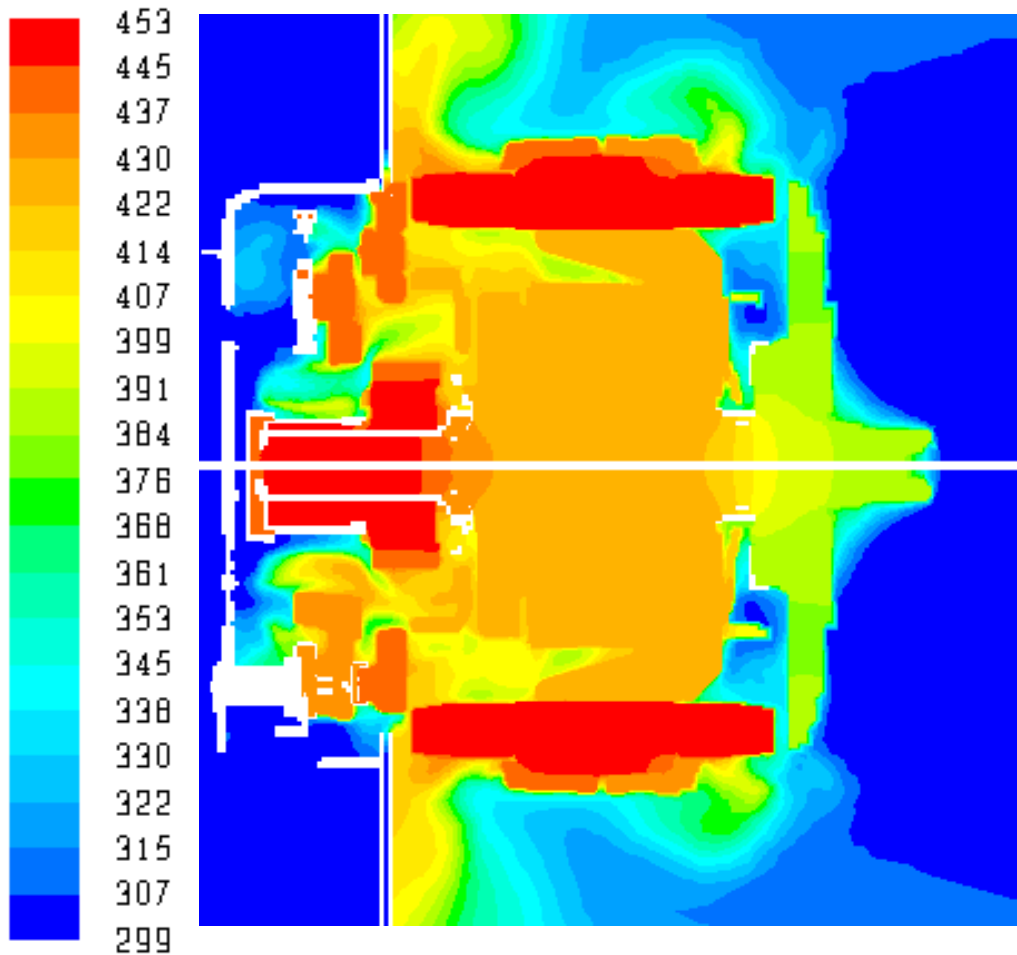


Velocity



Flow Rate (CFM)	Pressure Drop (in. water)	
	Experiment	Simulation
2.0	0.075	0.087
3.0	0.11	0.13
5.0	0.195-0.225	0.247

Simulations vs. Experiments



	Simulation	Test results
Stator copper	453	471
Stator iron	450	456
Front bearing	391	366
Rear bearing	450	389
diodes	440	418

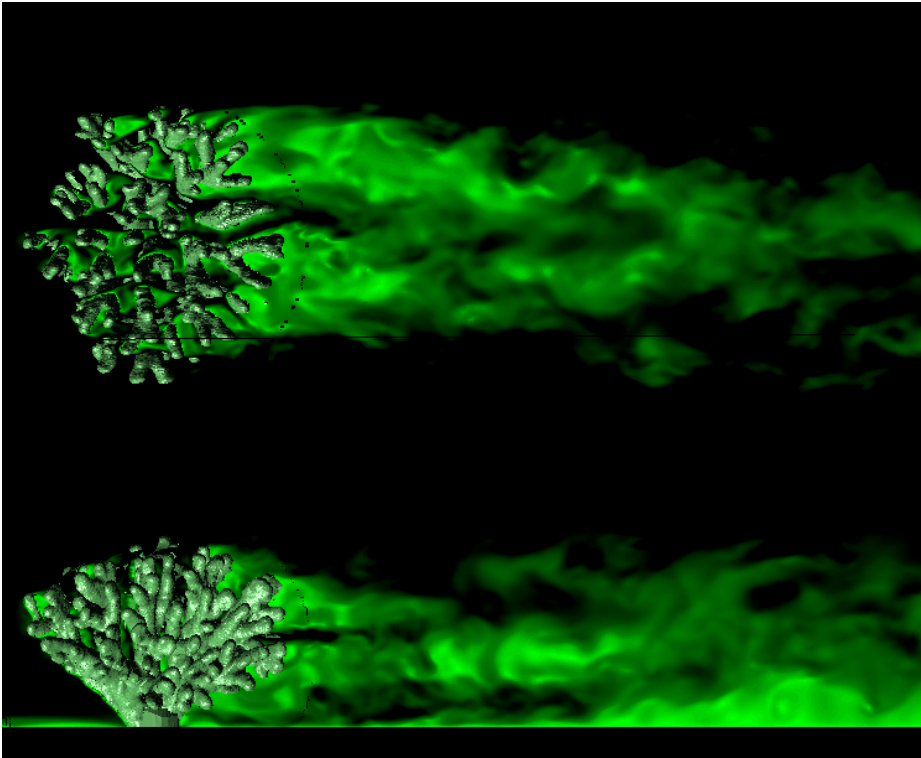
Temperature

7. Closing

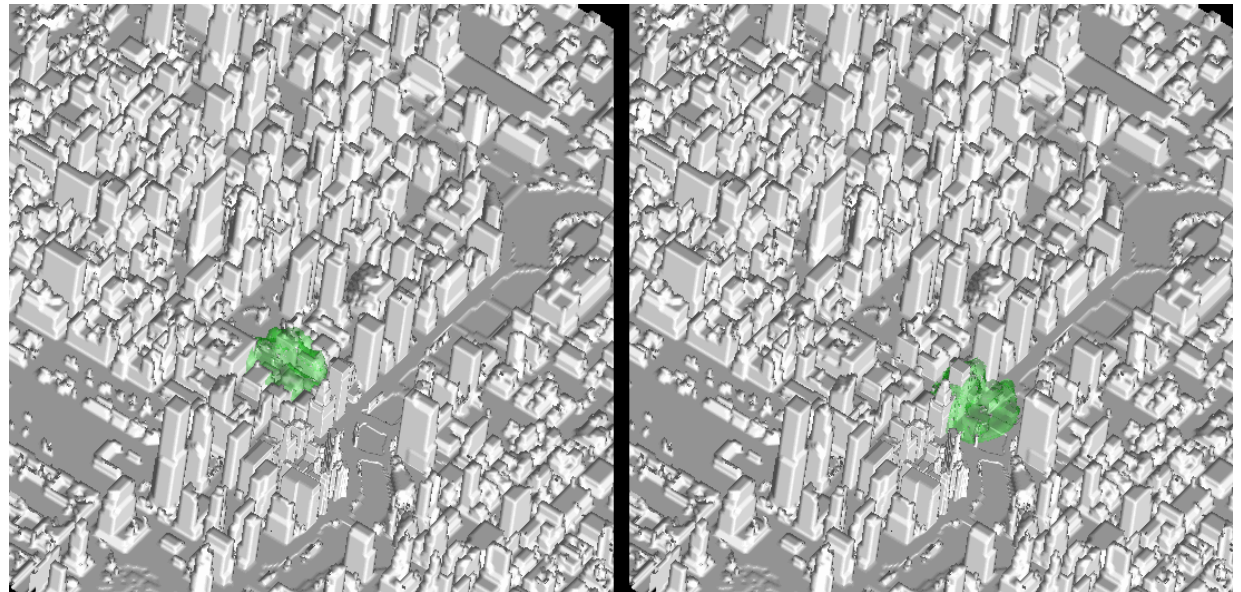
Solid/Fluid Thermal Coupling
Using the Immersed Boundary Method

Beyond CHT

Nutrient Transport in
Coral Reefs



Hazard Dispersion
In Urban
Environments



References

General Review: Mittal & Iaccarino, Ann. Rev. Fluid Mech. Vol. 37, pp. 239-261, 2005.

Review focused on turbulence: Iaccarino & Verzicco, Applied Mechanics Review, Vol. 56, No. 3, pp. 331-347, 2003.

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IB for Compressible RANS: de Tullio, Iaccarino, et. al. J. Comp. Physics, Vol. 225, pp. 2098–2115, 2007.

IB Reconstructions: Kang, Moin, Iaccarino, AIAA J., Vol. 47, No. 7, pp. 1750-1760, 2009.

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G. Kalitzin, S. Das, D. Cook

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Thank You